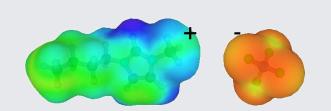


## Capture of Pollutants from Post-Combustion Streams with Ionic Liquids





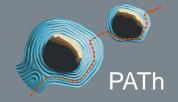


#### Luís M. C. Pereira

luismanuel@ua.pt

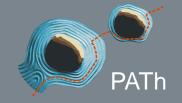
20 de Julho de 2012





- **1.** General Introduction
  - **1.1. Air Pollution**
  - **1.2.** Ionic Liquids
  - **1.3. Soft-SAFT EoS**
  - **1.4.** Scope and Objectives
- 2. Molecular Models
- **3.** Gas Solubilities
- **4.** ILs' Capturing Efficiency and Selectivities
- **5.** Conclusions
- 6. Future Work

### **1. General Introduction** 1.1 Air Pollution



*"contamination of the indoor or outdoor environment by any chemical, physical or biological agent that modifies the Natural characteristics of the atmosphere"* 



#### N<sub>2</sub>O anthropogenic source:

-Agriculture – 57% -Chemical industry – 29% -Transport – 5%

**WHO** 

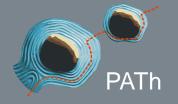
#### NO<sub>x</sub> anthropogenic sources:

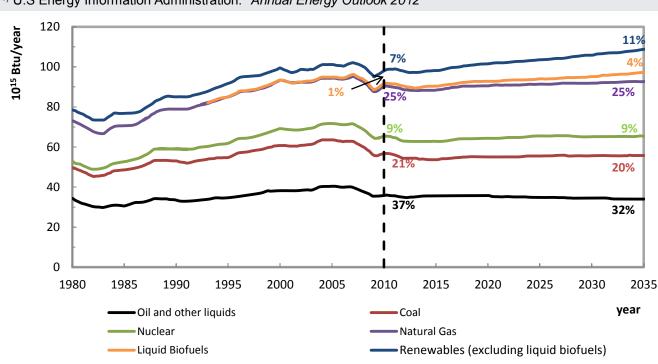
-Fossil fuel Combustion - 61% (Coal-fired electric power plants and industrial combustion)

#### **Control Methods:**

- Process optimization
- Thermal decomposition
- Selective Non Catalytic Reduction (SNCR) 10-90%
- Selective Catalytic Reduction (SCR) 80-95%
- Low-NO<sub>x</sub> burner (LNB) 14-65%
- Over Fire Air (OVA) +10-25%

### **1. General introduction** 1.1 Air Pollution





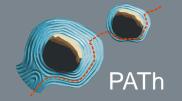
<sup>1)</sup> U.S Energy Information Administration. "Annual Energy Outlook 2012"

- Dependency on fossil fuels will continue
- Stricter legislation will continue appearing
- Need for better and more efficient control methods

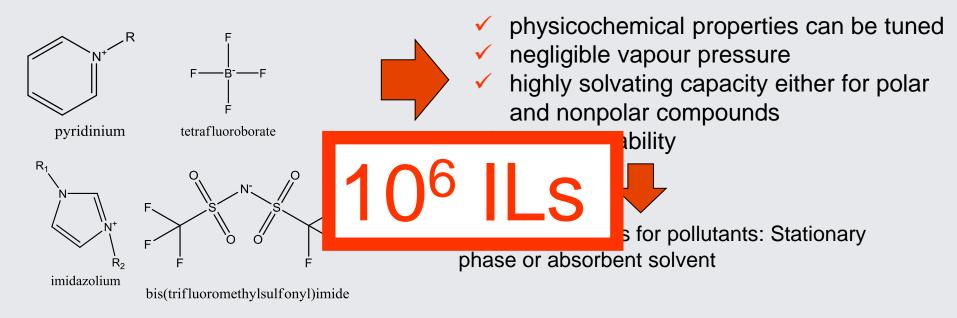


Ionic Liquids (ILs) as capturing agents

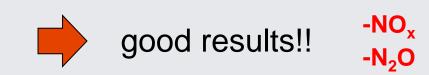
#### **1. General introduction** 1.2 Ionic Liquids



"salts composed of large organic cations and organic or inorganic anions that cannot form an ordered crystal and thus remain liquid at or near room temperature"



Pollutants solubility in ILs, namely for  $CO_2, CH_4, H_2S, SO_2, CO$  and  $NH_3$ 

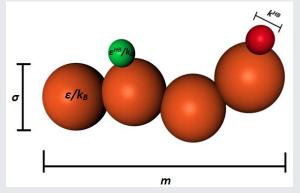


#### **1. General Introduction 1.3 Soft-SAFT EoS**

#### SAFT- Statistical Associating Fluid Theory

✓ Soft-SAFT EoS

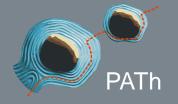
<sup>2)</sup> Vega et al., J. Ind. Eng. Chem. Res., **1998**. **37**(2): p. 660-674.



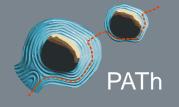
$$\sigma_{ij} = \eta_{ij} \frac{\sigma_{ii} + \sigma_{jj}}{2}$$
$$\varepsilon_{ij} = \xi_{ij} \sqrt{\varepsilon_{ii} \times \varepsilon_{jj}}$$

-Useare lue sphedeale fluig (asi so fail reference fluide cular parameters (m,  $\sigma$ ,  $\varepsilon/k_B$ ,  $\varepsilon^{HB}/k_B$  and kuses statistical mechanisms to calculate totabea ergivest interactionse (modeogen **boradimet**ers ( $m, \sigma, \varepsilon/k_B, Q$  and  $x_p$ ). -do not require ILs' critical properties

$$Q = Q_{exp} \times x_p$$

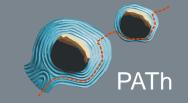


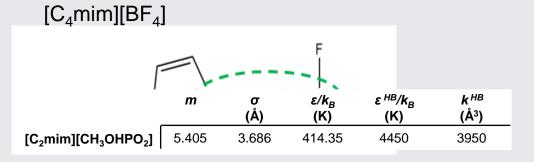
$$A^{res} = A^{ref} + A^{chain} + A^{assoc} + A^{polar}$$



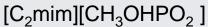
- Solubility measurement of CO<sub>2</sub>, N<sub>2</sub>O, N<sub>2</sub> and CH<sub>4</sub> in a Highly polar IL ([C<sub>2</sub>mim][CH<sub>3</sub>OHPO<sub>2</sub>])
- Soft-SAFT modelling of the measured data and extension to others Gas + IL systems
- Gas selectivies
- ILs' capturing efficiency compared to other solvents

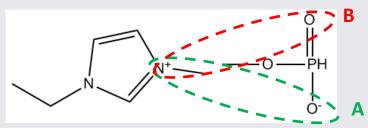
#### **2. Molecular Models** 2.1 Molecular models for the ILs

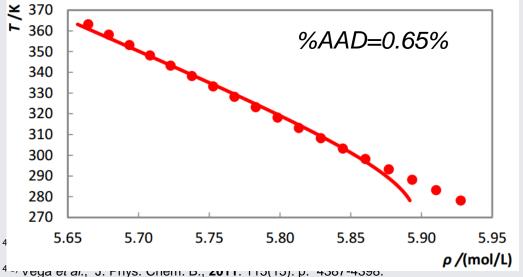




<sup>3)</sup> Vega et al., J. Phys. Chem. C., **2007**. 111(43): p. 16028-16034.





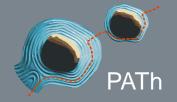


 $T=0.7 \times \epsilon/k_B$ 

<sup>5)</sup> Johnson *et al.*, Mol. Phys., **1993**. 78(3): p. 591-618

T=290.05 K

#### **2. Molecular Models** 2.2 Molecular models for the Gases



0===0		т	σ (Å)	ε/k <sub>B</sub> (K)	<i>Q</i> (10 <sup>-40</sup> C. m <sup>2</sup> )	$x_p$
000	CO <sub>2</sub>	1.571	3.184	160.20	4.4	1⁄3
<sup>6)</sup> Pedrosa <i>et al.,</i> Ind. Eng. Chem. Res., <b>2005</b> . 44(17): p. 7027-7037.	N <sub>2</sub>	1.205	3.384	89.16	1.2	1⁄2
<sup>7)</sup> Dias <i>et al.,</i> Ind. Eng. Chem. Res., <b>2006</b> . 45(7): p. 2341-2350.	CH4	1.000	3.728	147.20	-	-

#### Adjusted molecular parameters for N<sub>2</sub>O

Set	т	σ (Å)	ε/k <sub>B</sub> (K)	<b>x</b> <sub>p</sub>	Q (10 <sup>-40</sup> C. m²)	AAD P (%)	AAD D (%)
4	1.656	3.153	159.83	1⁄3	4.1	7.32	3.37

<sup>6)</sup> Pedrosa *et al.*, Ind. Eng. Chem. Res., **2005**. 44(17): p. 7027-7037.





<sup>2)</sup> Vega *et al.,* J. Ind. Eng. Chem. Res. **1998**. **37**(2): p. 660-674.

<sup>8)</sup> Pàmies et al., Ind. Eng. Chem. Res., **2001**. 40(11): p. 2532-2543.

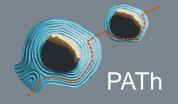
1<sup>st</sup> Approno quadrement

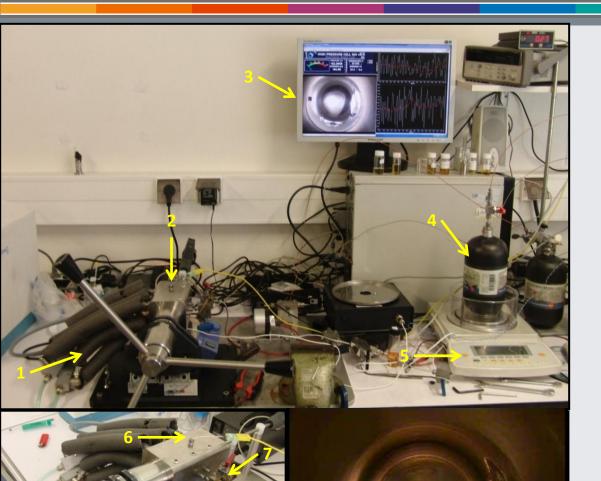
2<sup>nd</sup> Approach:

-modelled as three segments with the quadrupole moment in one of them ( $x_p$  fixed to  $\frac{1}{3}$ )



### **3. Gas Solubilities** 3.1 Experimental Equipment





- 1. Thermostatized bath circulator;
- 2. High pressure cell;
- 3. Video and data acquisition;
- 4. Gas storage;
- 5. Analytical balance;
- 6. Temperature sensor;
- 7. Valves;
- 8. Magnetic stirrer;
- 9. Piezoresistive pressure transducer;
- 10. Gas entrance;
- 11. Magnetic bar;
- 12. Light source from an optical fiber cable;
- 13. Pressure probe.

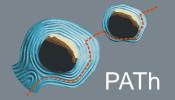
0-100 MPa

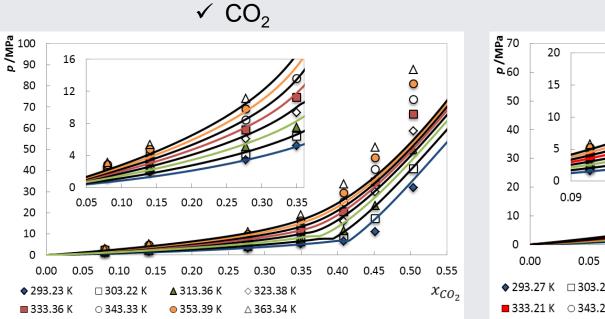
293-363 K

Solubility of  $CO_2$ ,  $N_2O$ ,  $CH_4$  and  $N_2$  in:

[C<sub>2</sub>mim][CH<sub>3</sub>OHPO<sub>2</sub>]

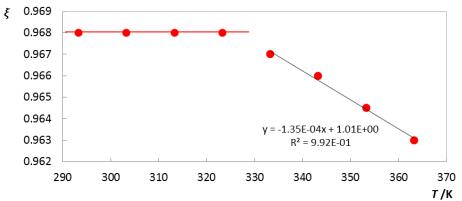
### **3. Gases Solubilities** 3.2 Experimental results





$$\xi = 1.017$$
 (T independent)

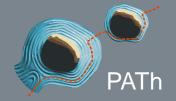
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0
 0

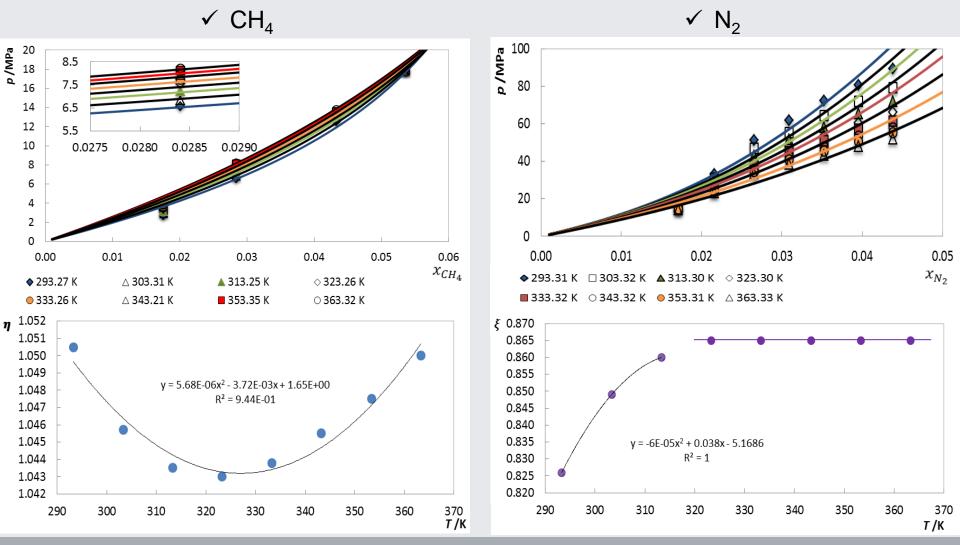


✓ N<sub>2</sub>O

11

## **3. Gases Solubilities3.2 Experimental results**

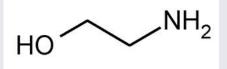




12

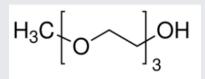
# 4. ILs' Capturing Efficiency and Selectivities

MEA - monoethanolamine



TEGMME - triethylene glycol monomethyl ether

U



$$S_{CO_2/N_2} = \frac{H_{N_2}}{H_{CO_2}}$$

$$S_{N_2O/N_2} = \frac{H_{N_2}}{H_{N_2O}}$$

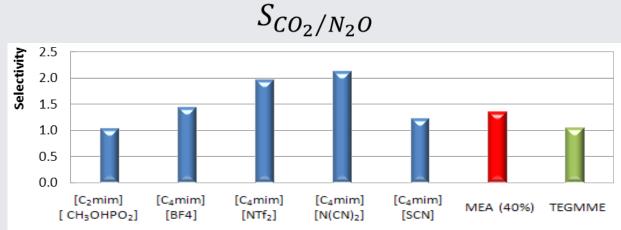
$$S_{CO_2/N_2O} = \frac{H_{N_2O}}{H_{CO_2O}}$$

$$MEA (40\%) TEGMME \ [C_2mim][CH_3OHPO_2] \ [C_4mim][N(CN)_2] \ [C_4mim][SCN] \ [C_4mim][BF_4] \ [C_4mim][Tf_2N]$$

$$CO_2 \ N_2O \ 102.78 \ 7.25 \ 18.34 \ 8.69 \ 12.78 \ 7.86 \ 3.21 \ 102.78 \ 7.86 \ 102.78 \ 7.86 \ 102.86$$

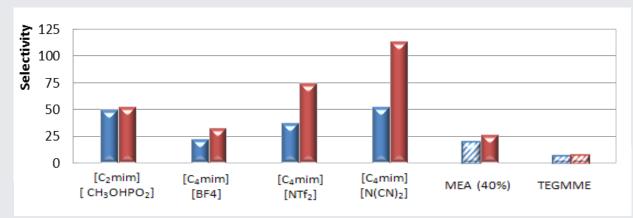
PATh

### 4. ILs' Capturing Efficiency and electivities



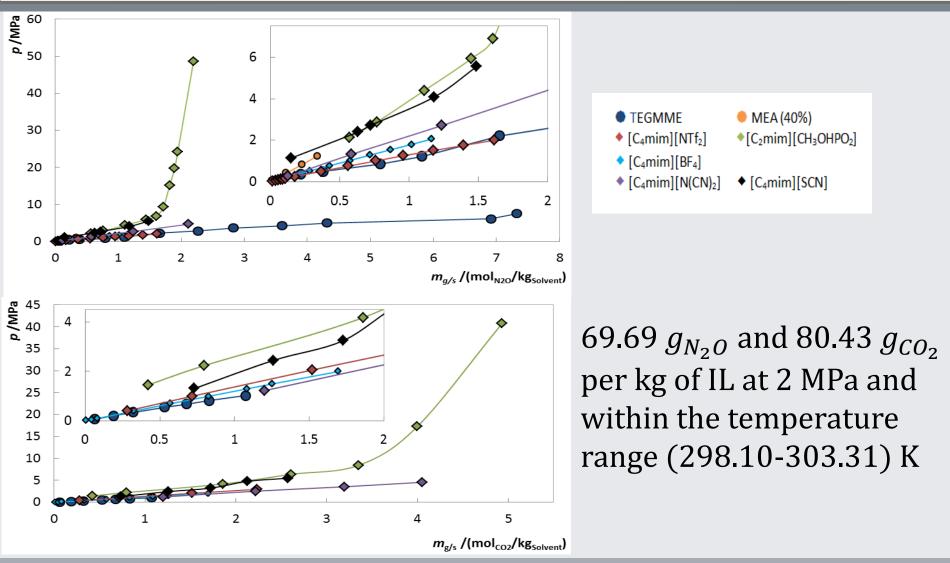
 $S_{N_2O/N_2}$ 

 $S_{CO_2/N_2}$ 



PATh

# 4. ILs' Capturing Efficiency and Selectivities

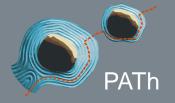


PATh

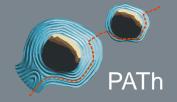
### **5.** Conclusions

- CO<sub>2</sub>, CH<sub>4</sub>, N<sub>2</sub> and N<sub>2</sub>O solubility in [C<sub>2</sub>mim][CH<sub>3</sub>OHPO<sub>2</sub>] was measured for the first time in a wide range of pressures and temperatures;
- Results showed a similar and high solubility of CO<sub>2</sub> and N<sub>2</sub>O in the ILs when compared to CH<sub>4</sub> and N<sub>2</sub>;
- Molecular parameters were proposed for N<sub>2</sub>O and the ILs [C<sub>2</sub>mim][CH<sub>3</sub>OHPO<sub>2</sub>], [C<sub>4</sub>mim][N(CN)<sub>2</sub>] and [C<sub>4</sub>mim][SCN];
- Soft-SAFT EoS was able to describe/predict pure compounds and binary mixtures successfully;
- Soft-SAFT EoS can be used as a prediction tool for pre-selection of the better ILs to dissolve some gases;
- ILs high selectivity toward CO<sub>2</sub> and N<sub>2</sub>O and high absorption capacity make them feasible candidates to be used to capture or separate these pollutants from post-combustion streams.





- Gases solubilities in other ILs (anion and alkyl chain effect)
- ✓ Solubility of other gases in ILs (O₂, O₃, HCI, HF, dioxins and furans)
- Extend soft-SAFT EoS to the measured systems



# Thank you for your attention!!

