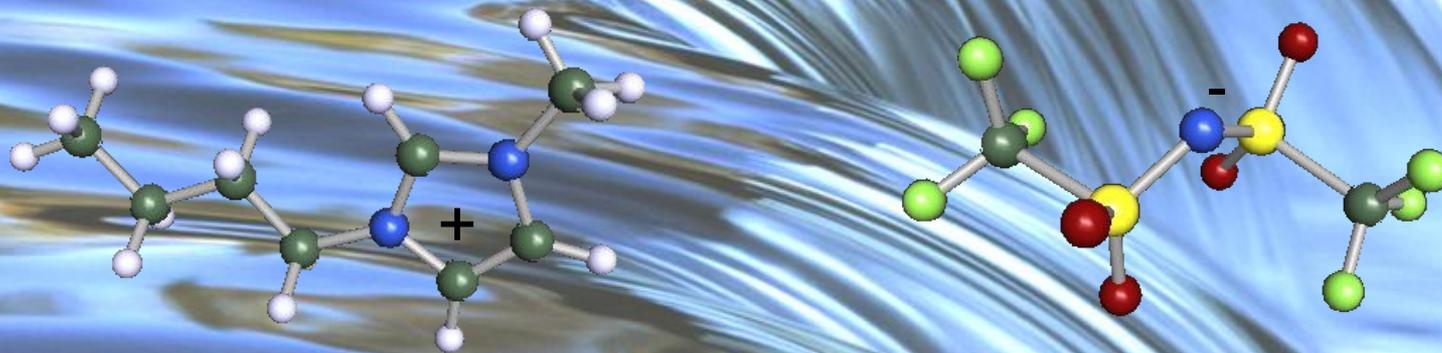


Treatment of Aqueous Effluents Contaminated with Ionic Liquids



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1. Introduction

- 1.1 ILs – Properties
- 1.2 ILs – Applications
- 1.3 Work Motivations

2. Methods to remove ILs from Water

- 2.1 Water Treatment Methods
- 2.2 Proposed Methods for Water Treatment

3. Materials and Results

- 3.1 Materials - Adsorption
- 3.2 Adsorption Results
 - 3.2.1 Alkyl side chain length
 - 3.2.2 Isomers
- 3.3 Materials - ABS
- 3.4 ABS Results
 - 3.4.1 ABS measurements
 - 3.4.2 Recovery efficiency
- 3.5 Process proposal

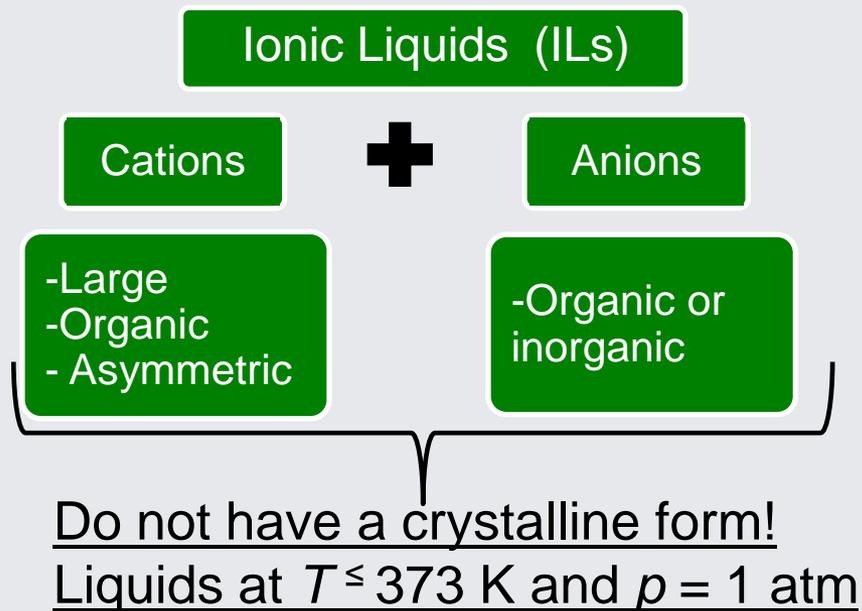
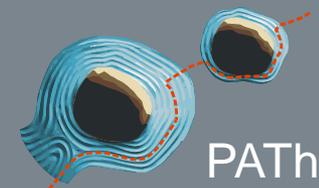
4. Conclusions

5. Future work



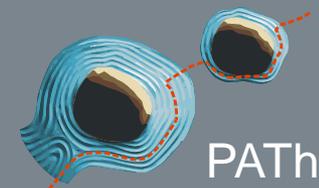
1. Introduction

1.1 ILs – ILs properties



1. Introduction

1.1 ILs – ILs properties



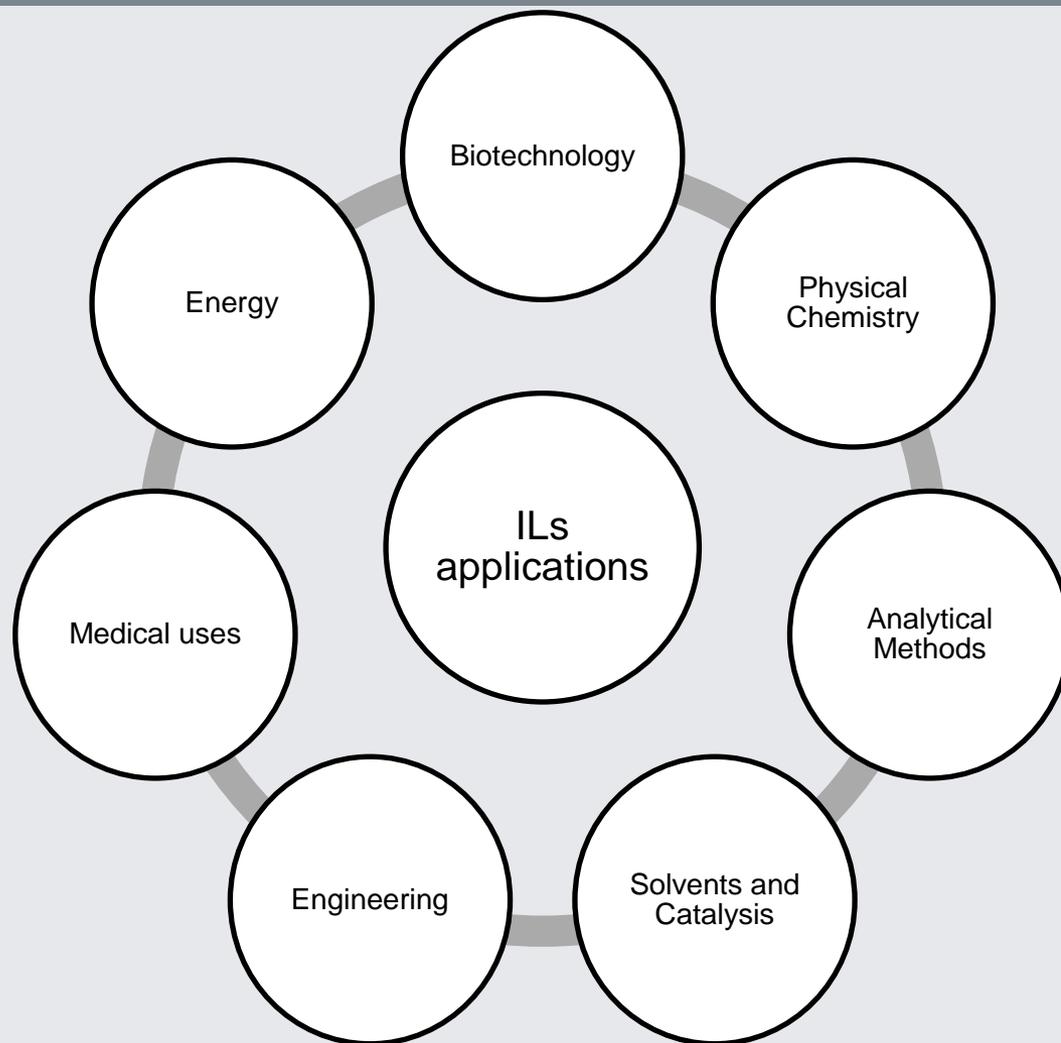
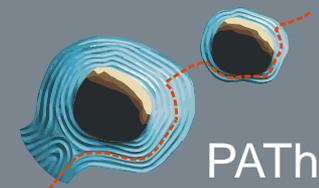
Property	ILs
Chemical stability	High
Thermal stability	High
Nº of Combinations	$> 10^6$
Melting Temperature	Low
Vapour Pressure	Low

“Designer solvents”

“Green solvents”

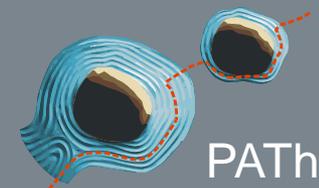
1. Introduction

1.2 ILs – ILs applications



1. Introduction

1.3 Work motivations



Toxicity tests with luminescent marine bacteria *Vibrio fischeri* (15 min)

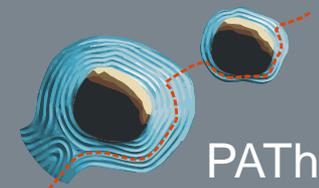
ILs	Log(EC ₅₀ / μM)	VOCs	Log(EC ₅₀ / μM)
[C ₄ mim][BF ₄]	3.55	Methanol	5.00
[C ₅ mim][BF ₄]	3.14	Acetone	4.29
[C ₆ mim][BF ₄]	2.15	Dichloromethane	3.40
[C ₇ mim][BF ₄]	2.44	Benzene	2.03
[C ₈ mim][BF ₄]	1.41	Toluene	1.50
[C ₉ mim][BF ₄]	0.72	Phenol	1.49
[C ₁₀ mim][BF ₄]	-0.18	O-Xylene	0.97
[C ₄ mim]Cl	2.95		
[C ₄ mim]Br	3.07		
[C ₄ py]Br	2.73		
[C ₄ mpy]Br	2.12		
[C ₆ mpy]Br	1.48		
[C ₈ mpy]Br	0.25		

Annotations: A yellow box labeled "Lower log(EC₅₀)" with a downward arrow points to the ILs column. A yellow box labeled "Higher Toxicity" with a downward arrow points to the VOCs column.

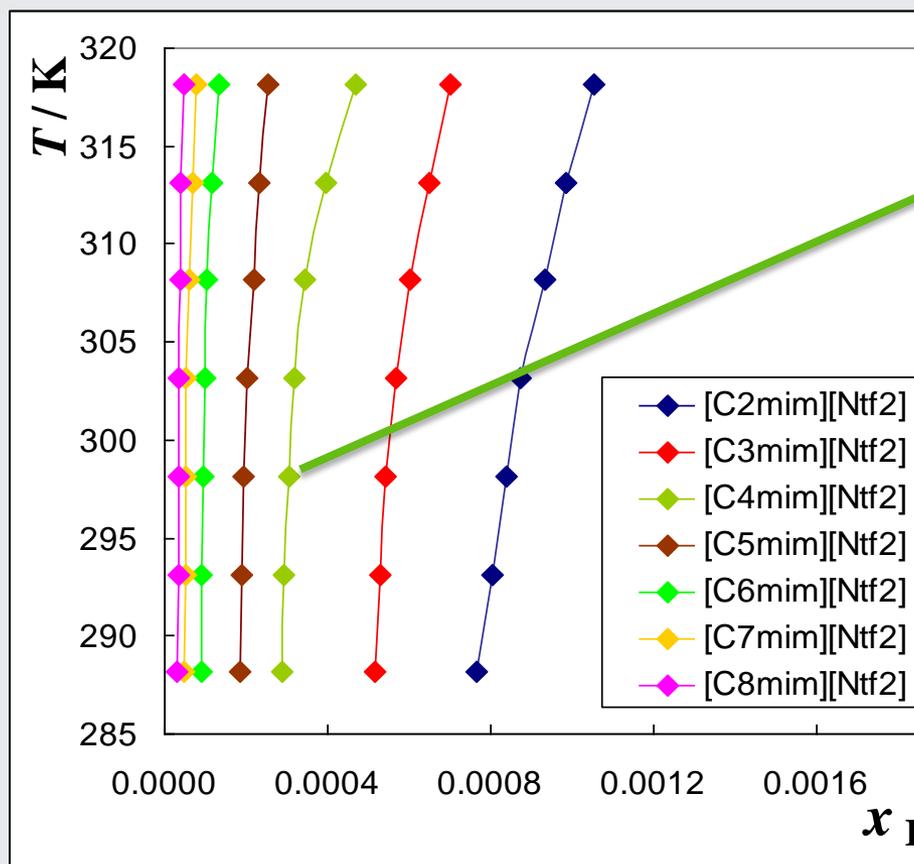
*J. Kärkkäinen, Master Thesis, Department of Chemistry, University of Oulu, Finland, 2007.

1. Introduction

1.3 Work motivations



Non-negligible solubility in water* (even those considered hydrophobic)



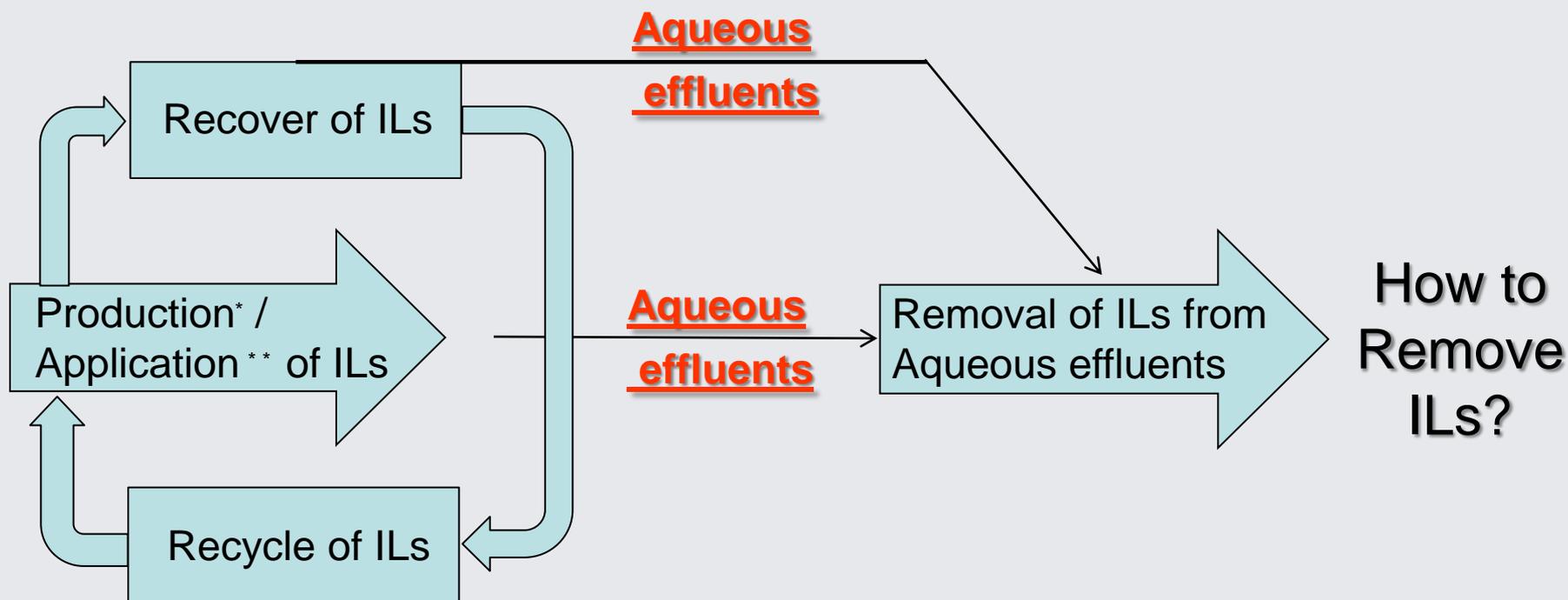
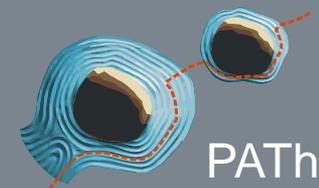
≈ 0.72 wt %

Use in a **large scale** leads to **aquatic environmental impact**

*M. G. Freire, C. M. S. S. Neves, P. J. Carvalho, R. L. Gardas, A. M. Fernandes, I. M. Marrucho, L. M. N. B. F. Santos, and J. A. P. Coutinho, *The Journal of Physical Chemistry B*, vol. 111, pp. 13082-13089, 2007.

1. Introduction

1.3 Work motivations

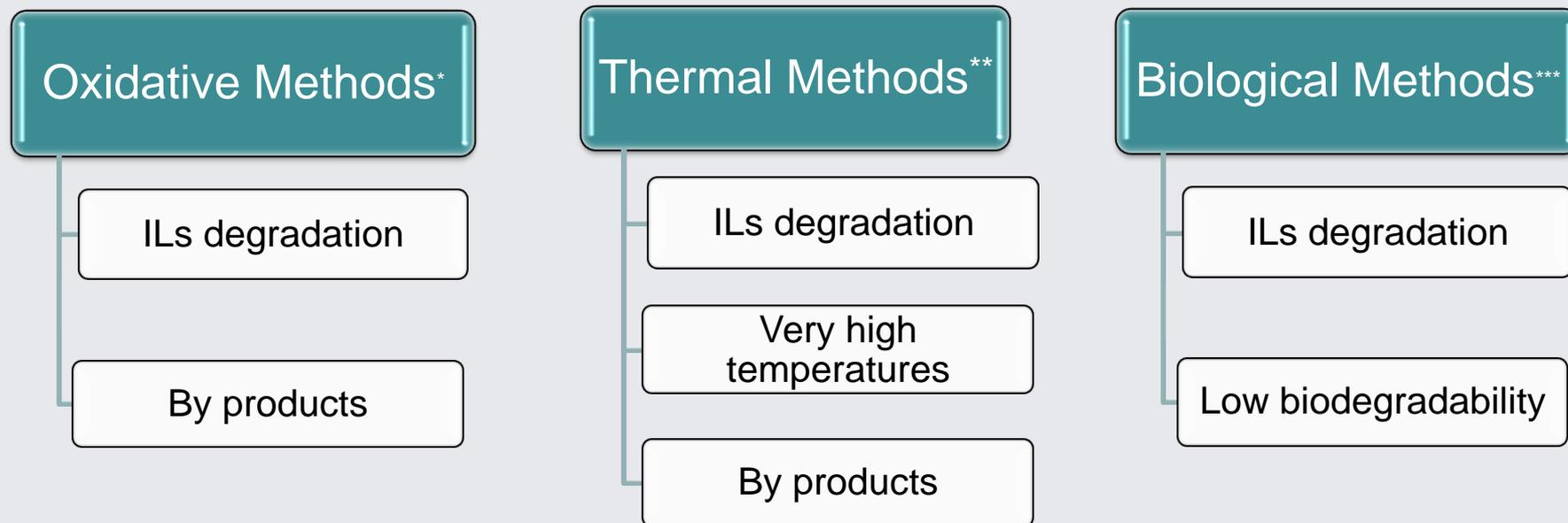
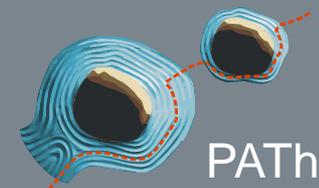


*P. T. Anastas, P. Wasserscheid, and A. Stark, *Handbook of Green Chemistry, Volume 6: Ionic Liquids*, 2010

**A. Kokorin, *Ionic Liquids: Theory, Properties, New Approaches*. InTech, 2011

2. Methods to remove ILs

2.1 Water treatment methods



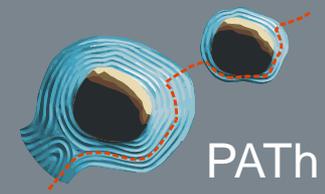
*T. P. Thuy Pham et al., *Water Research*, vol. 44, pp. 352-372, 2010

**A. Kokorin, *Ionic Liquids: Theory, Properties, New Approaches*. InTech, 2011

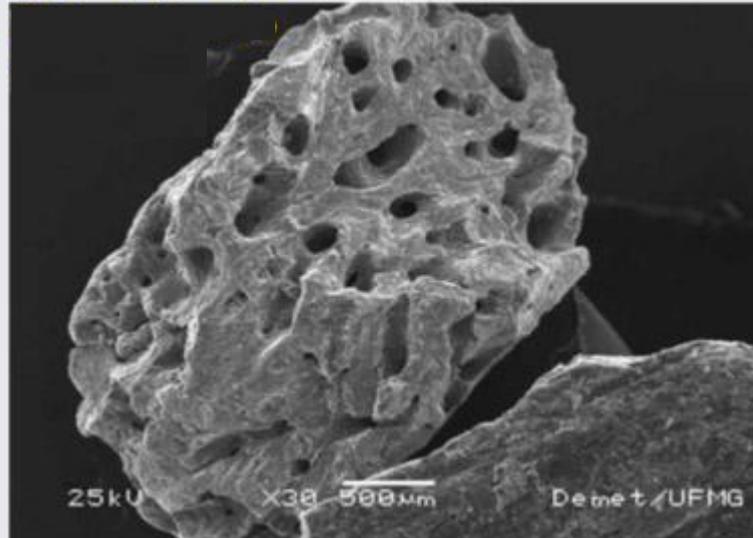
***C. Abrusci, et al., *Green Chemistry*, vol. 13, pp. 709-717, 2011

2. Methods to remove ILs

2.1 Proposed methods to water treatment



Adsorption for **Hydrophobic** ILs onto Activated Charcoal



□ Highly developed porosity

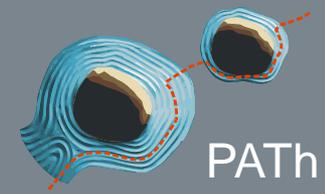
□ High surface area

□ Special surface reactivity

□ Highly inert

□ Thermally stable

2. Methods to remove ILs



2.1 Proposed methods to water treatment

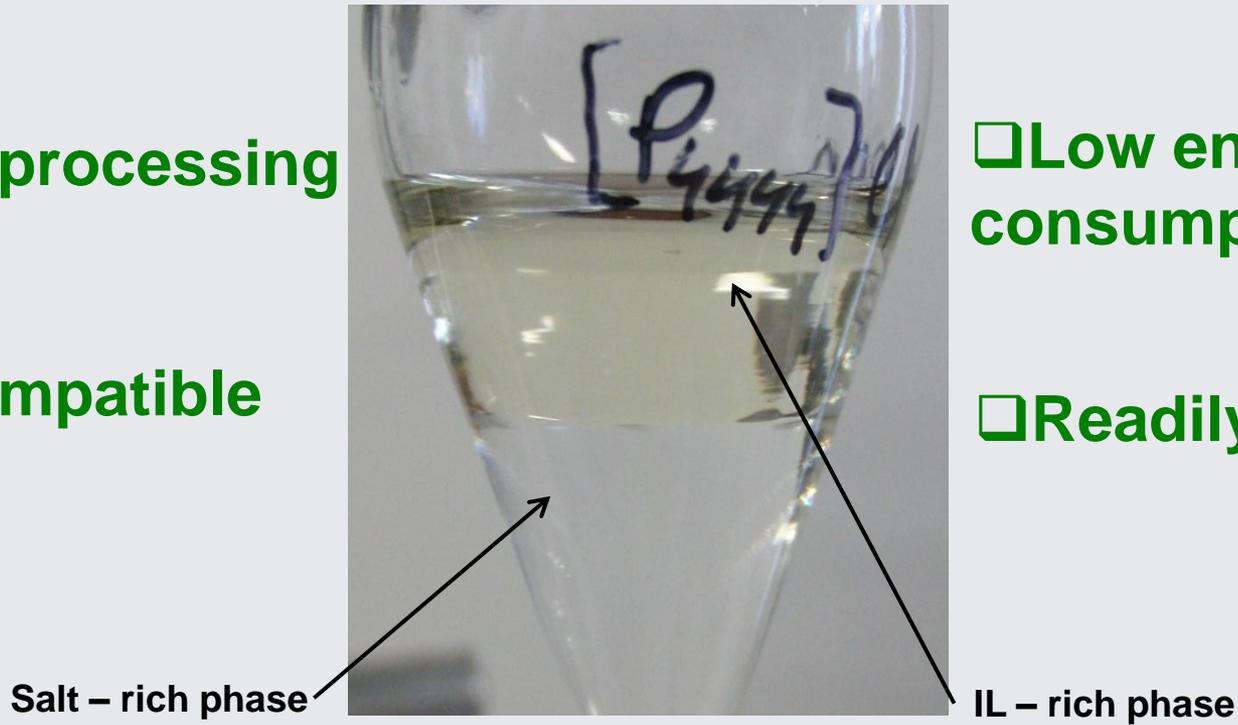
Aqueous Biphasic Systems (ABS) for **Hydrophilic** ILs

Short processing time

Biocompatible

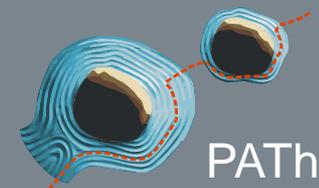
Low energy consumption

Readily scaled up

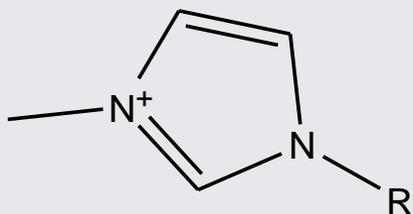


3. Materials and Results

3.1 Materials - Adsorption

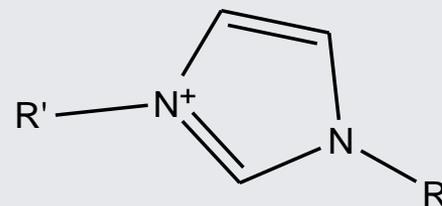


$C_n C_1 im$ series

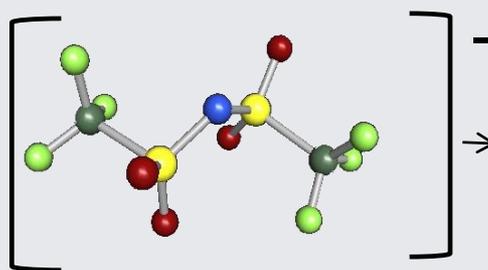


$R = 1,2,3,4,5,6,8,12$

$C_m C_m im$ series



$R' = 1,2,3$



Based ILs

bis(trifluoromethylsulfonyl)amide \blacktriangleright $[NTf_2]^-$

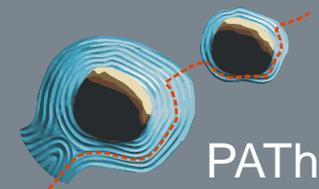
Activated Charcoal



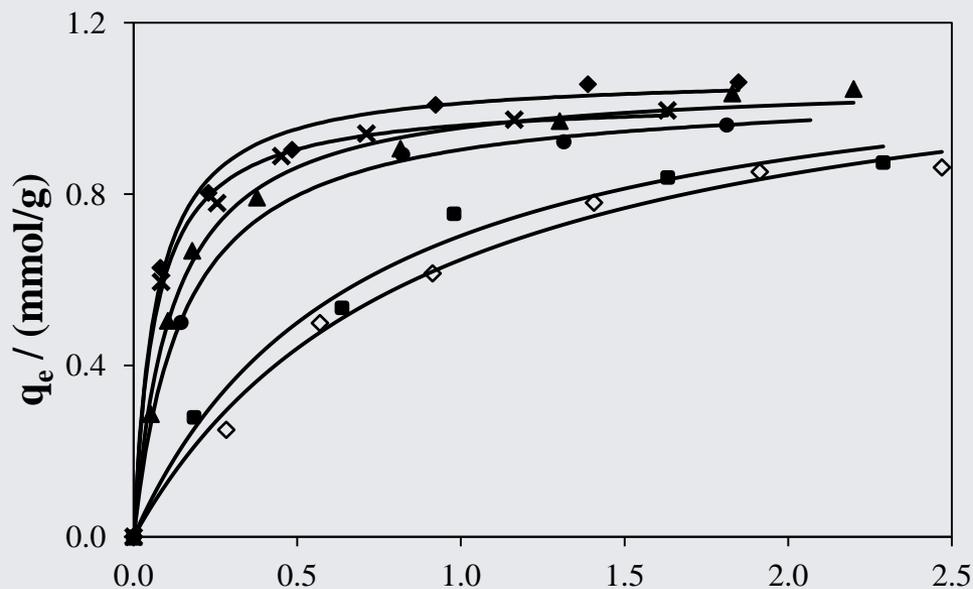
$T = 308 \text{ K}$

3. Materials and Results

3.2.1 Adsorption – Alkyl side chain length

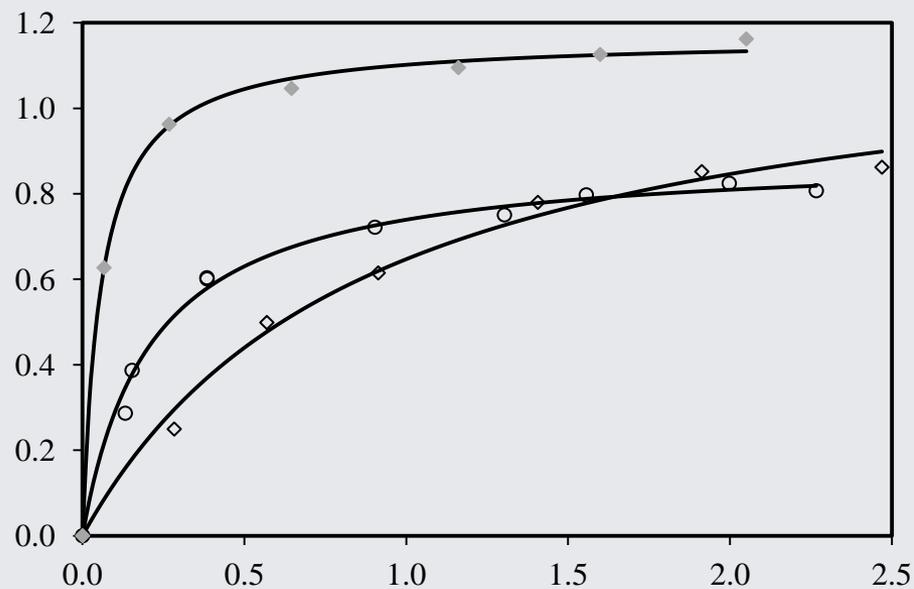


$C_n C_1$ im series



and

$C_m C_m$ im series:

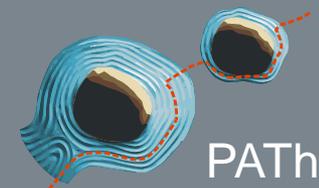


$C_e / (\text{mmol/L})$

(\diamond) [$C_1 C_1$ im], (\blacksquare) [$C_2 C_1$ im], (\bullet) [$C_3 C_1$ im], (\blacktriangle) [$C_4 C_1$ im], (\blacklozenge) [$C_5 C_1$ im], (\times) [$C_6 C_1$ im]; (\circ) [$C_2 C_2$ im][NTf₂], (\blacklozenge) [$C_3 C_3$ im][NTf₂]

3. Materials and Results

3.2.1 Adsorption – Alkyl side chain length



C_nC₁im series

and

C_mC_mim series:

IL	K _d / (L/kg)
[C ₁ C ₁ im] ⁺	512.6
[C ₂ C ₁ im] ⁺	540.8
[C ₃ C ₁ im] ⁺	621.9
[C ₄ C ₁ im] ⁺	660.2
[C ₅ C ₁ im] ⁺	689.1
[C ₆ C ₁ im] ⁺	653.7
[C ₈ C ₁ im] ⁺	601.1
[C ₁₂ C ₁ im] ⁺	546.3

IL	K _d / (L/kg)
[C ₁ C ₁ im] ⁺	512.6
	545.9
	748.0

Higher adsorption

Decrease in adsorption

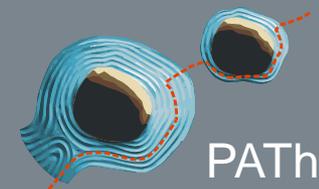
adsorption coefficient

× 1000

C_e (= 1.5 mmol/g)

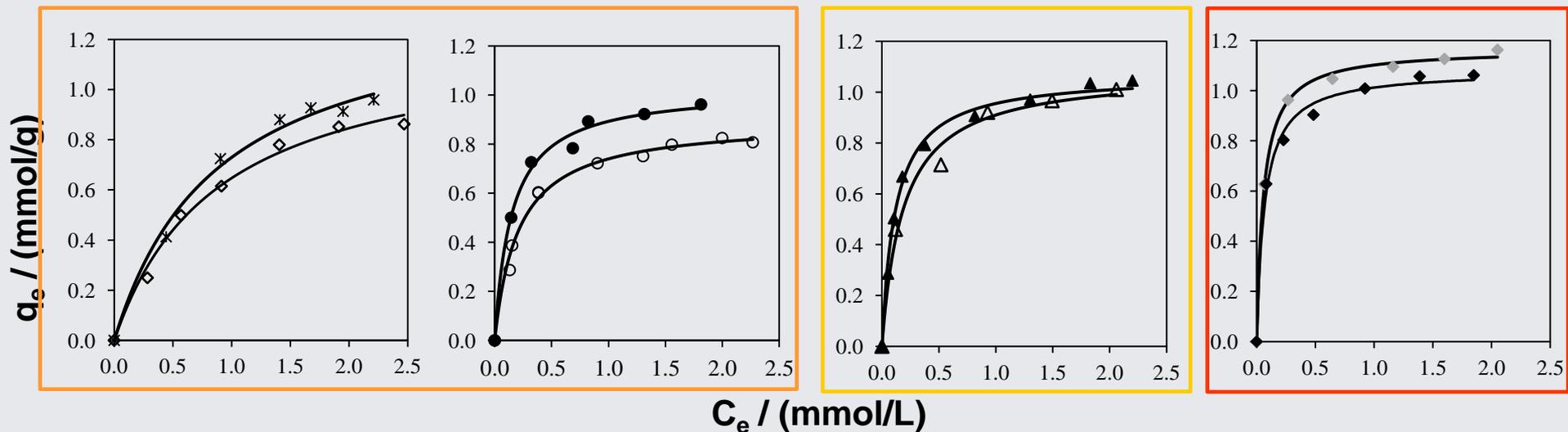
[C₁C₁im]⁺ < [C₂C₁im]⁺ < [C₃C₁im]⁺ < [C₄C₁im]⁺ < [C₅C₁im]⁺ < [C₆C₁im]⁺ < [C₈C₁im]⁺ < [C₁₂C₁im]⁺

3. Materials and Results



3.2.2 Adsorption – Isomers

Comparison between $C_m C_m$ im series and $C_n C_1$ im series:



(*) [C_2 im], (\diamond) [$C_1 C_1$ im]; b), (\bullet) [$C_3 C_1$ im], (\circ) [$C_2 C_2$ im], (\blacktriangle) [$C_4 C_1$ im], (\triangle) [$C_2 C_3$ im], (\blacklozenge) [$C_5 C_1$ im], (\blacklozenge) [$C_3 C_3$ im].

alkyl side chain length



$C_n C_1$

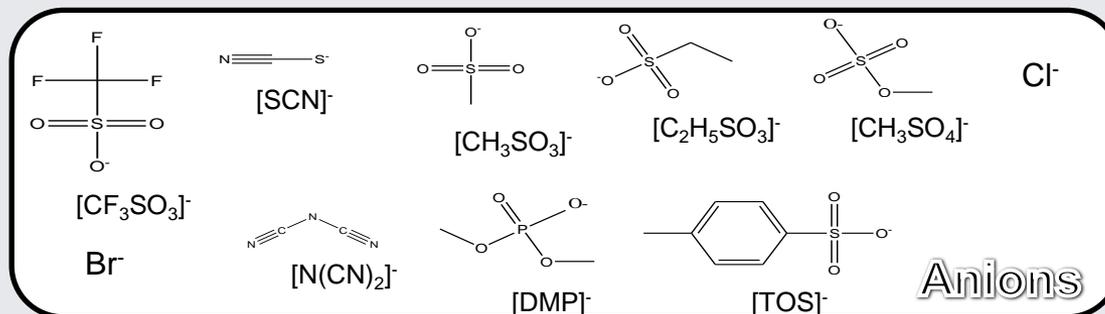
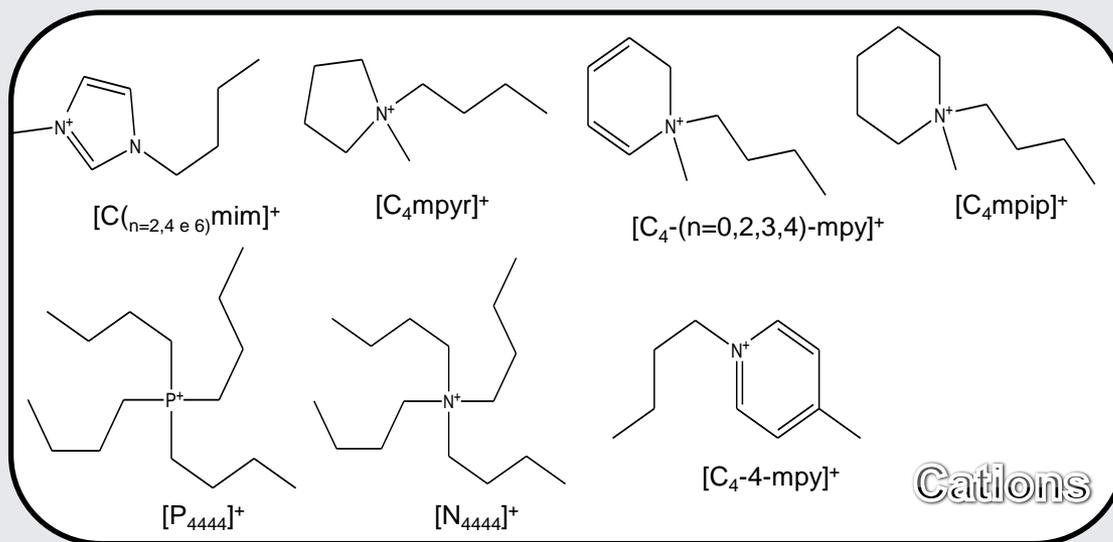
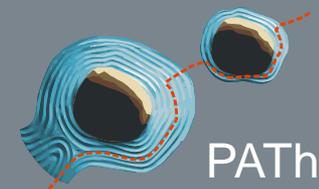
$C_m C_m$

$C_m C_m$

$C_n C_1$

3. Materials and Results

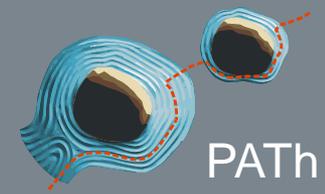
3.3 Materials- ABS



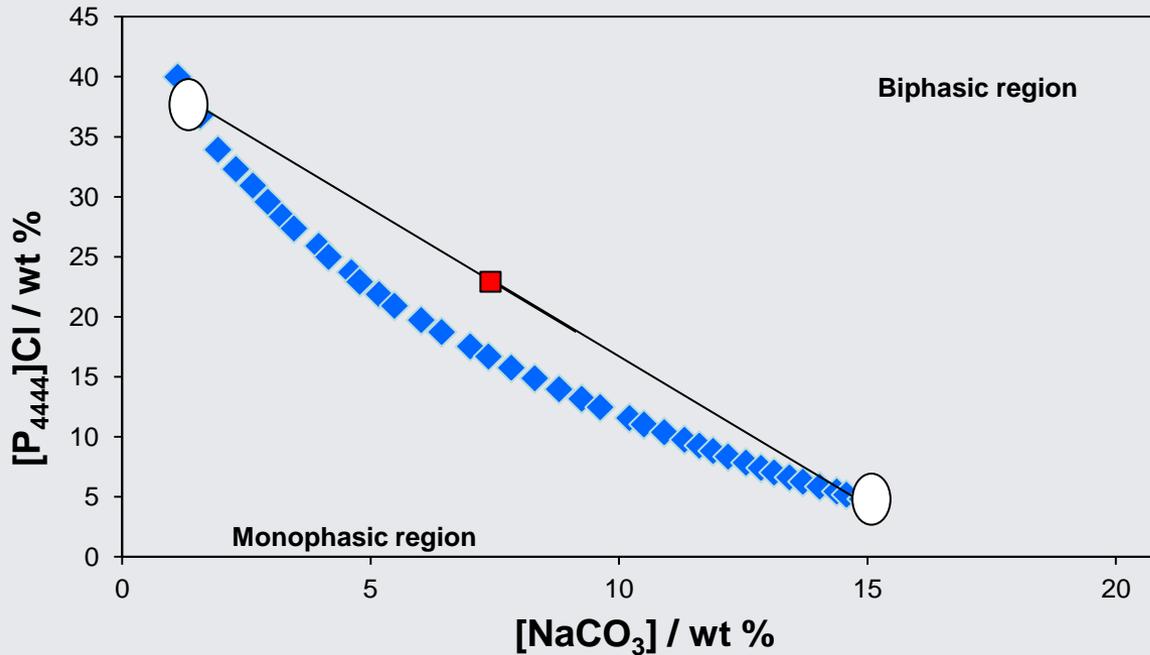
Na_2CO_3 as phase promoter agent due to its good salting-out ability

$T = 298 \text{ K}$

3. Materials and Results



3.4.1 ABS – Measurements

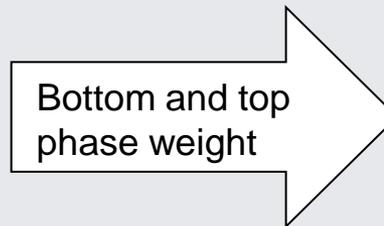
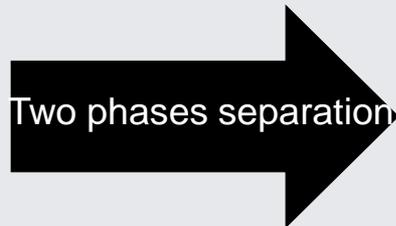
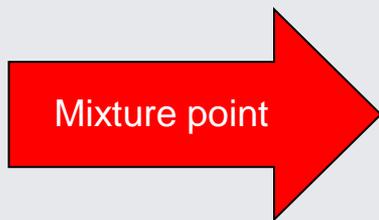


$$[IL]_T = A \times e^{(B \times [Salt]_T^{0.5} - (C \times [Salt]_T^3))}$$

$$[IL]_B = A \times e^{(B \times [Salt]_B^{0.5} - (C \times [Salt]_B^3))}$$

$$[IL]_T = \frac{[IL]_M}{\alpha} - \frac{1 - \alpha}{\alpha} \times [IL]_B$$

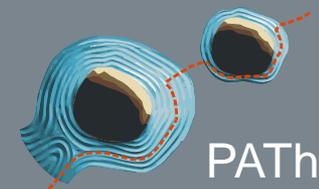
$$[Salt]_T = \frac{[Salt]_M}{\alpha} - \frac{1 - \alpha}{\alpha} \times [Salt]_B$$



Calculation of the bottom and top weight fractions by the *Merchuk* equation

3. Materials and Results

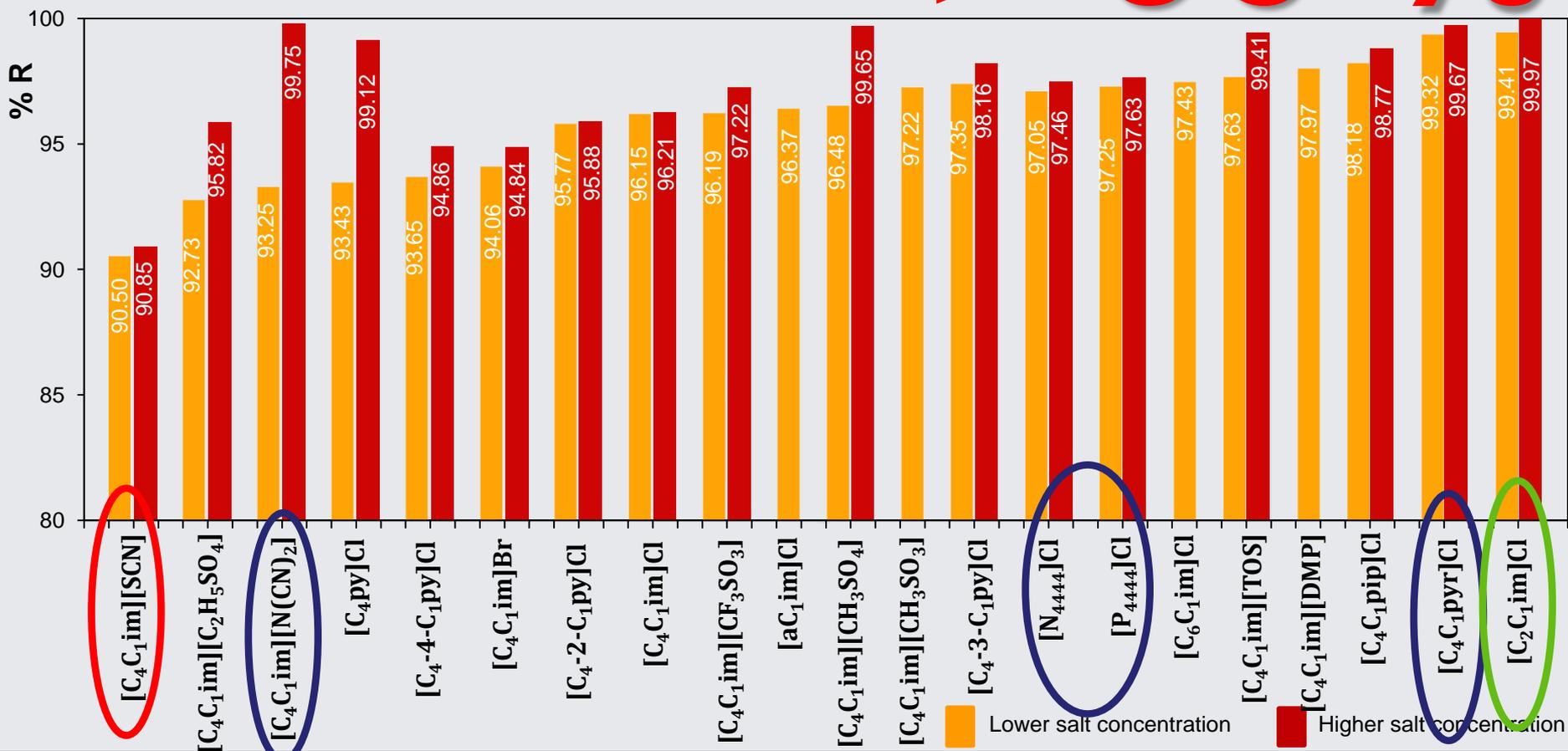
3.4.2 ABS – Recovery efficiency



$$\%R = \frac{[IL]_{IL} \times m_{IL}}{[IL]_{IL} \times m_{IL} + [IL]_{Salt} \times m_{Salt}} \times 100$$

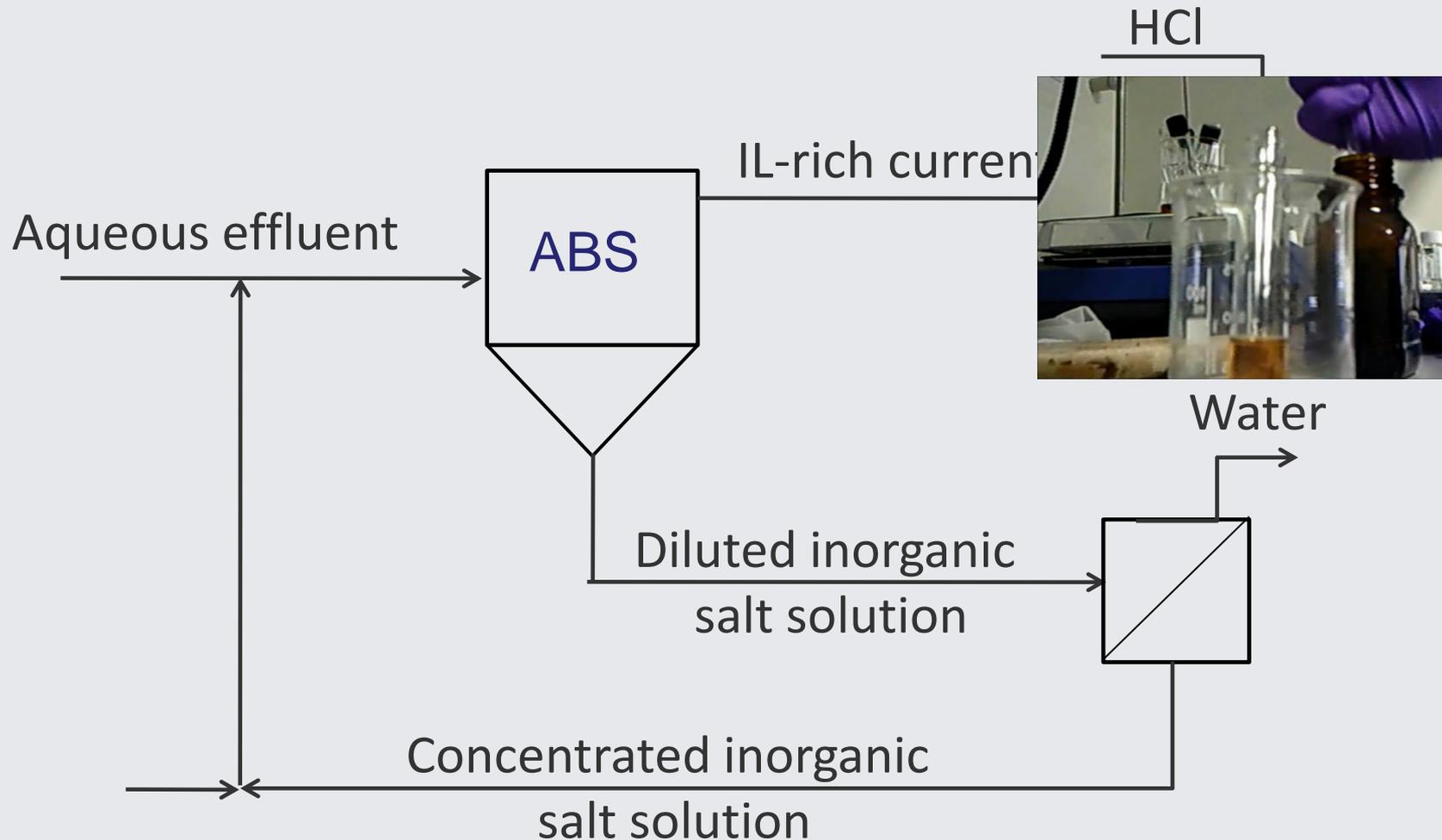
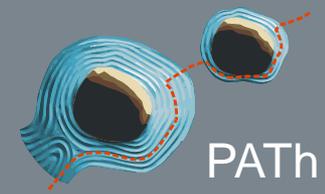
> 90%

Range	IL %	IL %
3.4	4.0	34.0

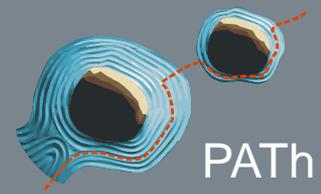


3. Materials and Results

3.5 Process proposal



4. Conclusions

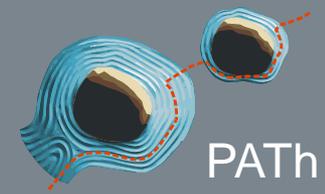


Adsorption of ILs onto AC is **effective** at low concentrations.

Adsorption **increases** with the alkyl side chain length increase for both series studied.

Aqueous Biphasic Systems are a potential asset for the ILs Recovery. The recovery efficiencies obtained were **always higher than 90%**.

5. Future Work



Adsorption:

- ❖ Recovery of ILs from AC (acetone*)
- ❖ ≠ anion families
- ❖ ≠ T e ≠ Adsorbents

ABS:

- ❖ Ionic exchange from the two salts
- ❖ ≠ salts with higher recovery efficiencies and low salt content

*J. Palomar, J. Lemus, M. A. Gilarranz, and J. J. Rodriguez, *Carbon*, vol. 47, pp. 1846-1856, 2009.

Acknowledgments

