

Development of a Solubility Parameters Scale for Ionic Liquids

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❖ Introduction

- ❖ Biofuels

- ❖ Ionic Liquids

- ❖ Solubility Parameter

❖ Estimation of the Solubility Parameter

- ❖ Activity coefficients at infinite dilution

- ❖ Viscosity

❖ Experimental Section

❖ Conclusion

❖ Future work

❖ Acknowledgements

Introduction

► Bioethanol and Biobutanol – Work context



Bioethanol & Biobutanol

- ❖ Renewable resources
- ❖ Liquid transport fuels replacing the usual fuels
- ❖ Reduce emissions of hydrocarbon, carbon monoxide
- ❖ Improves the engine combustion

Introduction

► Bioethanol and Biobutanol

❖ The production of biofuels by fermentation requires a process for the recovery of alcohol from the aqueous medium



DISTILLATION



The presence of water will form an azeotrope with the alcohol

Introduction

► Extractive Distillation – Problem Resolution

- ❖ Azeotropic distillation
- ❖ Liquid-liquid extraction
- ❖ Pervaporation
- ❖ **Extractive distillation**



**Third component
added to the mixture**
– Change in the
relative volatility of
compounds

- organic solvent
- solid salt
- mixture
- **IONIC LIQUID**

Introduction

► Extractive Distillation with Ionic Liquids

IL as entrainer

- ❖ Breaking of azeotropes
- ❖ Less energy consumption
- ❖ Lower costs
- ❖ Lower capital investment

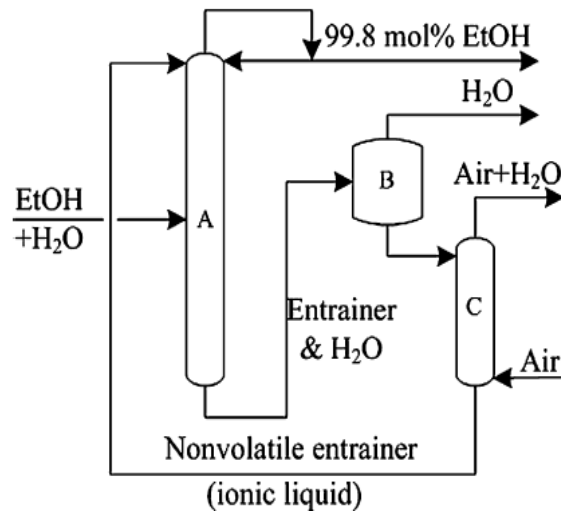
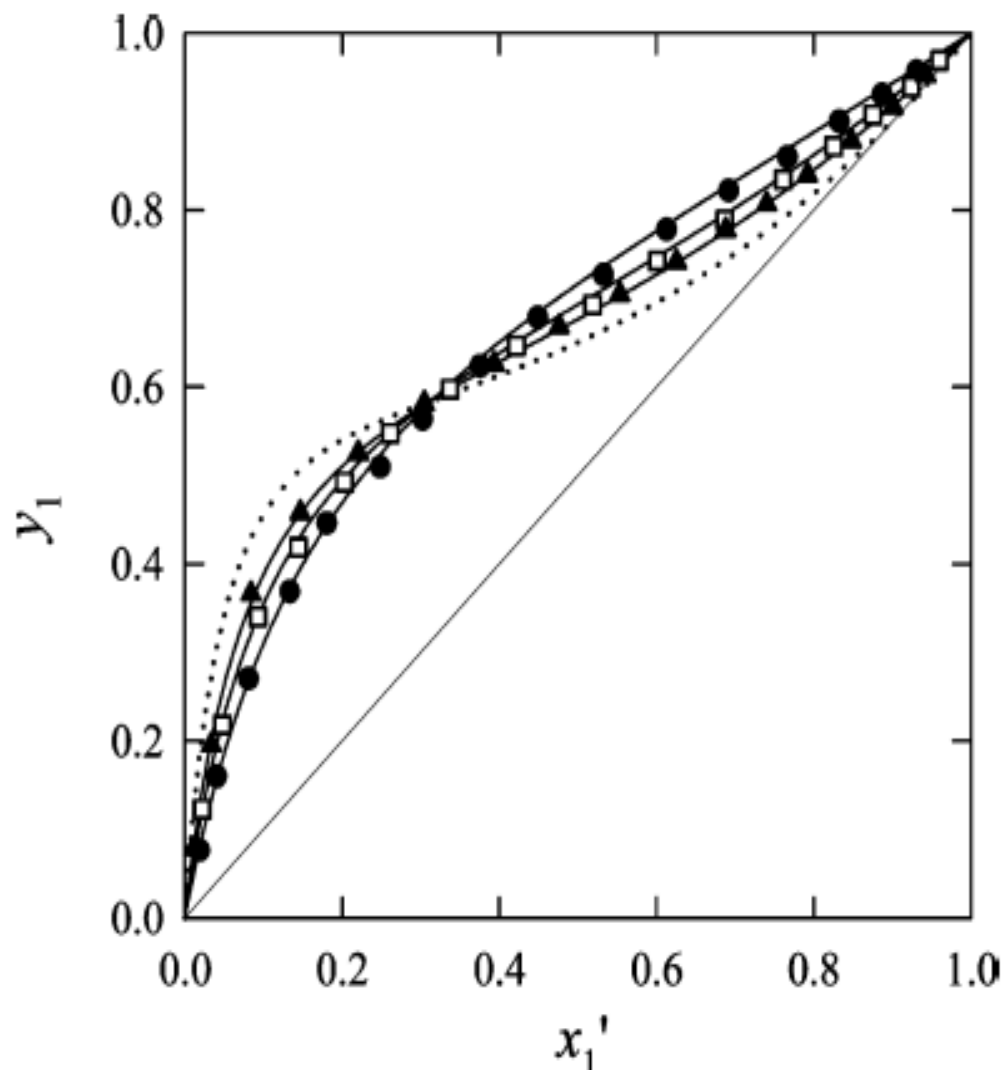
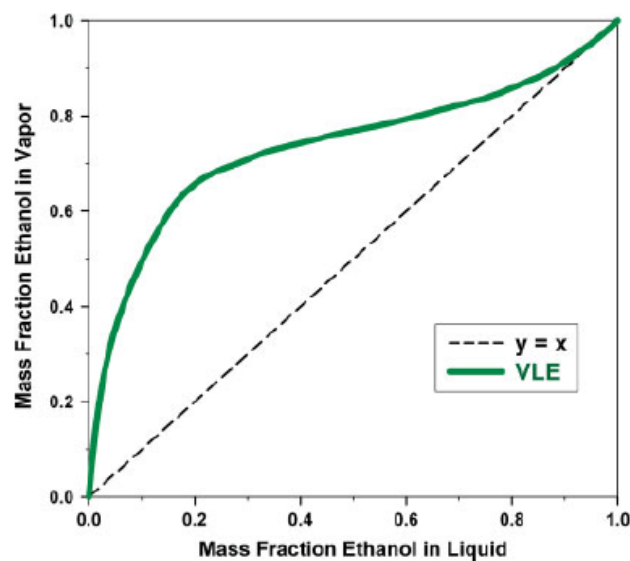


Fig. 14. Extractive distillation using ionic liquid as non-volatile entrainer (A: main column, B: flash drum, C: stripping column) [93].



Introduction

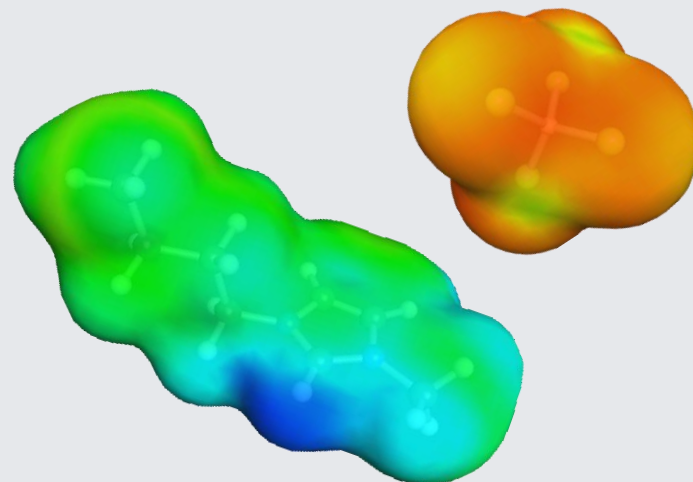
► Extractive Distillation with Ionic Liquids



Introduction

► Ionic Liquids

- ❖ **Molten salts**, liquid at room temperature
- ❖ **Bulky and Asymmetric** cation
- ❖ **Several** types of anion (halides, inorganic, organic)



- ❖ Low melting point ($<100^{\circ}\text{C}$)
- ❖ Non flammable
- ❖ Negligible vapor pressure
- ❖ Good thermal stability
- ❖ Possibility of tune their properties for specific task

Introduction

► Ionic Liquids

Task - specific

Properties are related to the cation and anion that built the Ionic Liquid:

- ❖ Hydrophobicity
- ❖ Viscosity
- ❖ Density

Structure – Property relations

Introduction

► Ionic Liquids

Large number of potential ILs → Unfeasibly to Study experimentally



Normally used:
Group contribution method

Predictive models

- Experimental Data
- Theory



Hildebrand solubility
parameter

Ionic Liquid as entrainer
Extractive Distillation

1 Introduction

► Solubility Parameter



Hildebrand

$$\delta = \left(\frac{\Delta U}{V} \right)^{1/2}$$

The Hildebrand theory was developed for **Regular Solutions**:

- Systems with negligible excess volume and excess entropy

$$G^E = U^E$$

Hildebrand and Scatchard equation for free Gibbs energy
Relation with solubility parameter

$$G^E = U^E = \Phi_1 \Phi_2 (\delta_1 - \delta_2)^2 (x_1 V_1 + x_2 V_2)$$

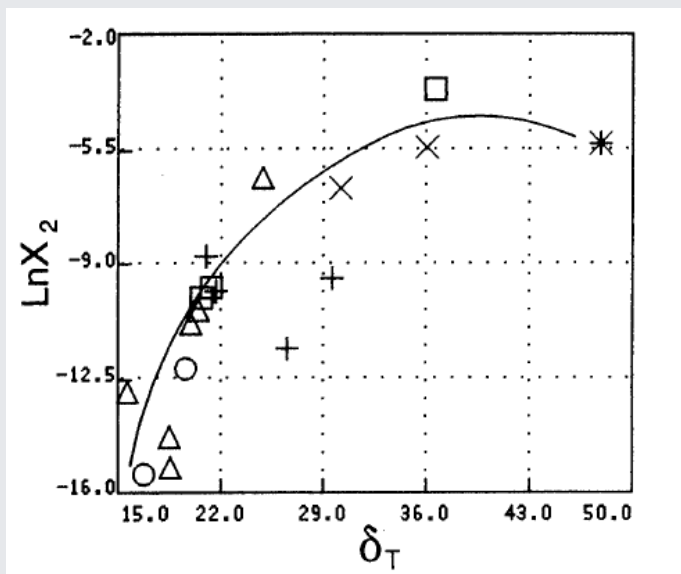
1 Introduction

► Solubility Parameter – estimation

To estimate the **solubility parameter** they suggested that experimental data according to:

$$\delta_i = \sqrt{\frac{\Delta U^{vap}}{V_i}} = \sqrt{\frac{\Delta H^{vap} - RT}{V_i}}$$

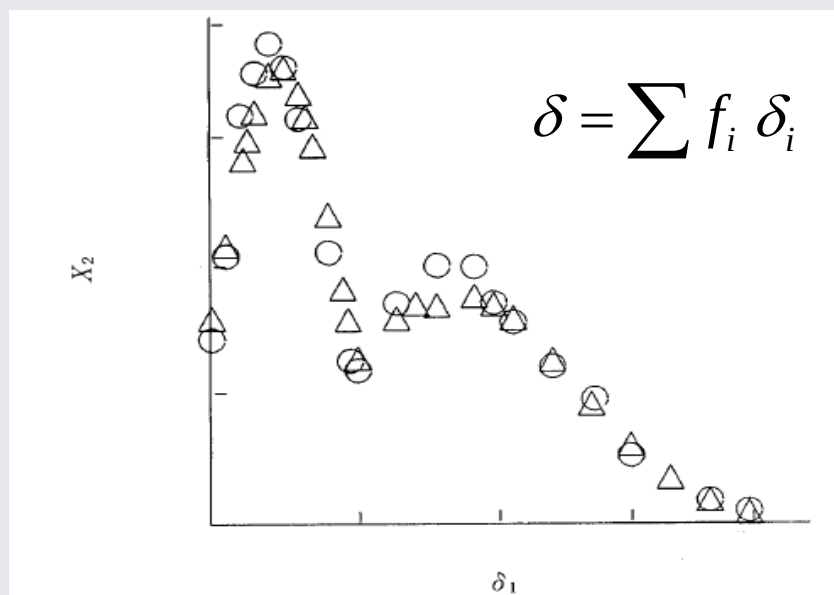
Or: using the **mole fraction solubility**



Maximum of solubility
corresponds to the value of the
overall solubility parameter for
the compound in study.

Introduction

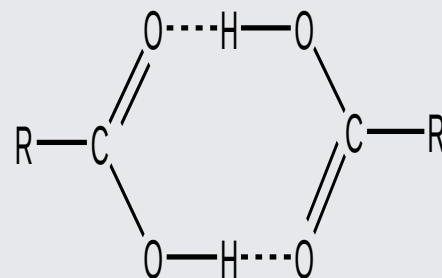
► Solubility Parameter



❖ Chamaleonic effect

Defined by Hoy:

- ➡
- **Two** different behaviours accordingly to the solvents present in the medium



Introduction

► Solubility Parameter

- How does solubility parameter helps on the process of Extractive distillation?

$$RT \ln(\gamma_j) = V_j \Phi_i^2 (\delta_i - \delta_j)^2$$

Regular Solution Theory

$$S_{ij} = \frac{\gamma_i}{\gamma_j}$$

Selectivity

Selectivity is an indicator of a promising solvent for one specific mixture

Introduction

► Solubility Parameters Scale – Aim of the project

Establishment of a solubility parameters scale

Choise of the best IL

Estimation of solubility parameters:

- Density
- **Viscosity**
- Surface tensions
- Lattice energy
- Melting points
- **Activity Coefficients at infinite dilution**

Estimation of Solubility Parameters

► Activity Coefficients at infinite dilution

One of the most important thermodynamic properties is the activity coefficient which is related to the excess free Gibbs energy by,

$$G^E = RT \sum_i x_i \ln(\gamma_i)$$

Combining:

- previous equation with the one obtained by Hildebrand for G^E with solubility parameter

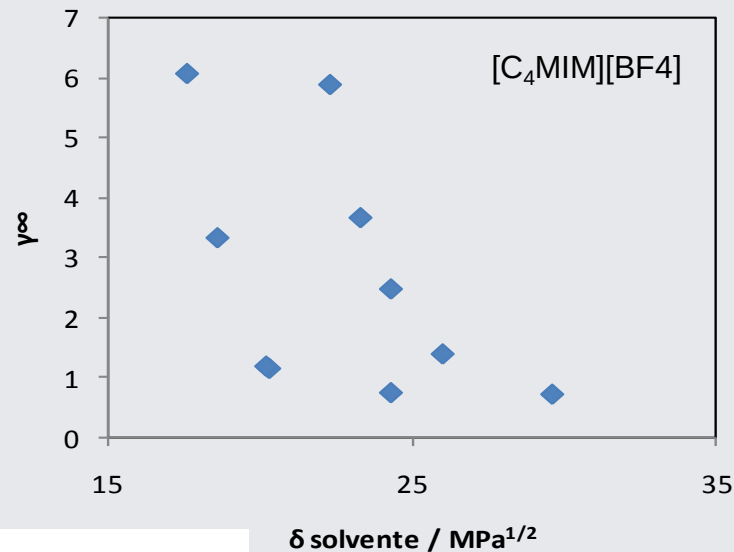
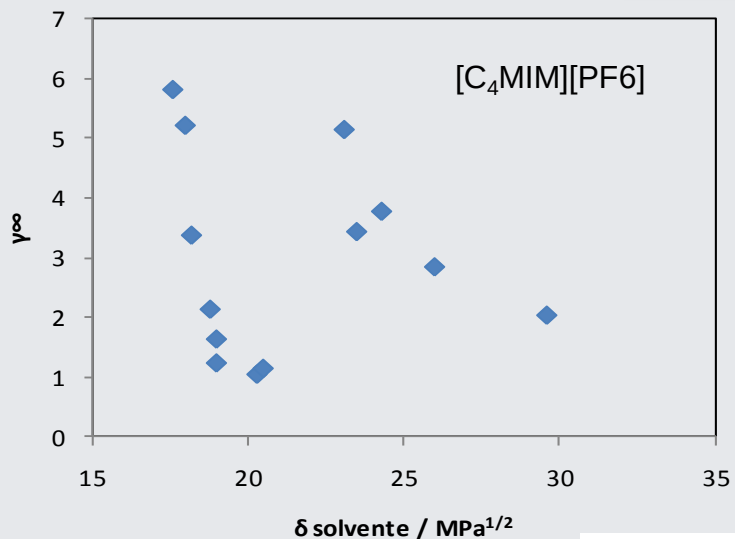
- Applying infinite dilution conditions, $\Phi_i=1$ and $\gamma_i = \gamma^\infty$

$$RT \ln(\gamma^\infty) = V_j (\delta_i - \delta_j)^2 \quad \rightarrow \quad \delta_i = \delta_j + \left(\ln(\gamma^\infty) \frac{RT}{V_j} \right)^{1/2}$$

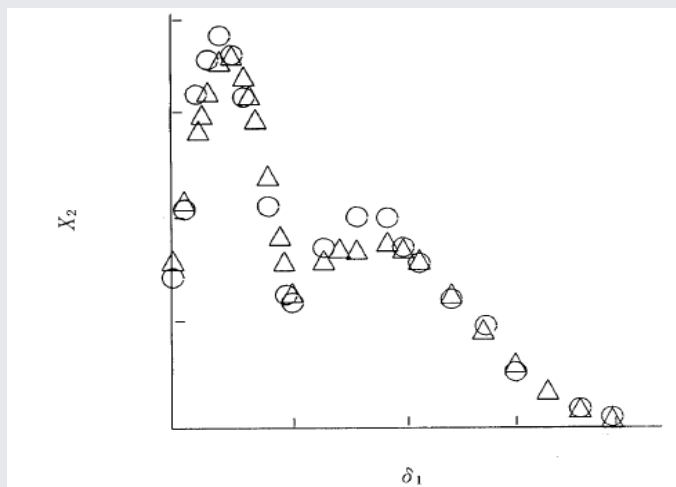
Estimation of Solubility Parameters

► Activity Coefficients at infinite dilution - Results & Discussion

Collected data



$$\gamma = \frac{1}{x}$$

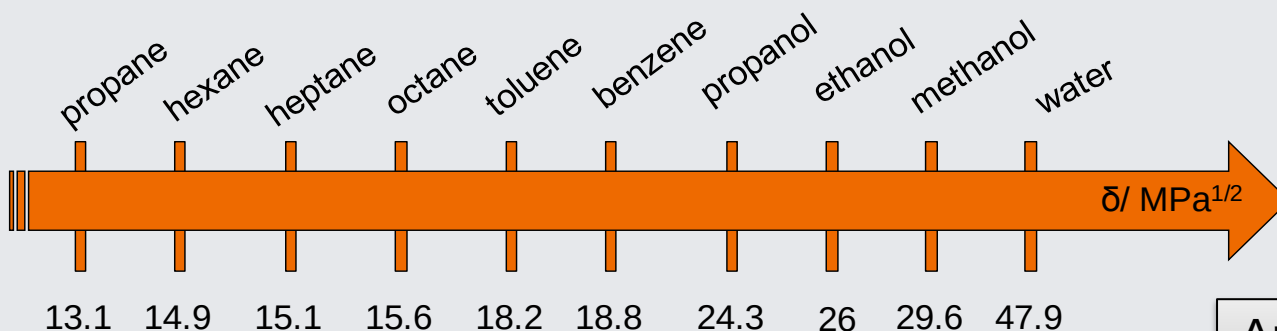
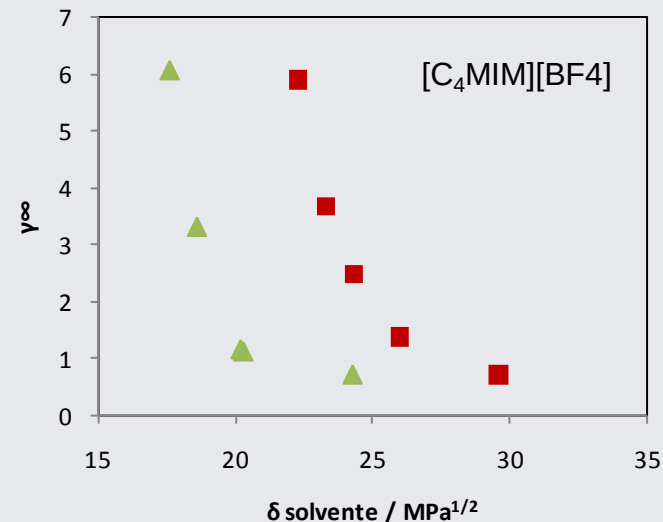
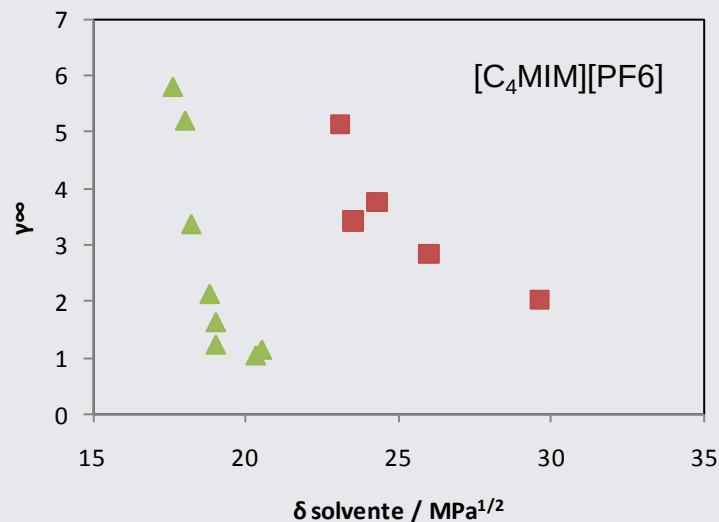


Chameleonic Effect

Estimation of Solubility Parameters

► Activity Coefficients at infinite dilution - Results & Discussion

Collected data



Amphiphilic Characteristic of
ILs

➤ Estimation for **two solubility parameters**:

δ_{NP} – NONPOLAR families;

δ_P – POLAR families

Temperature 298.15K

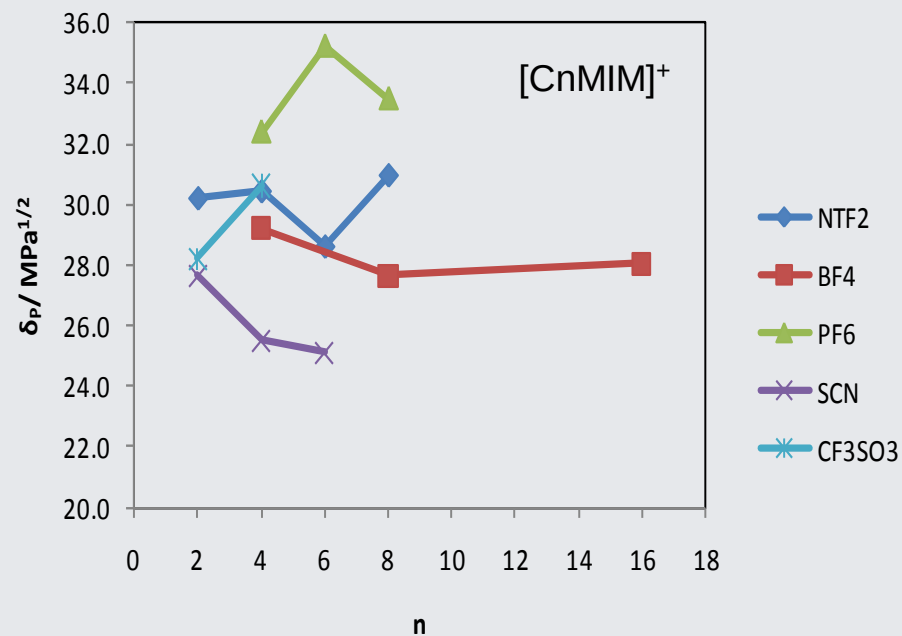
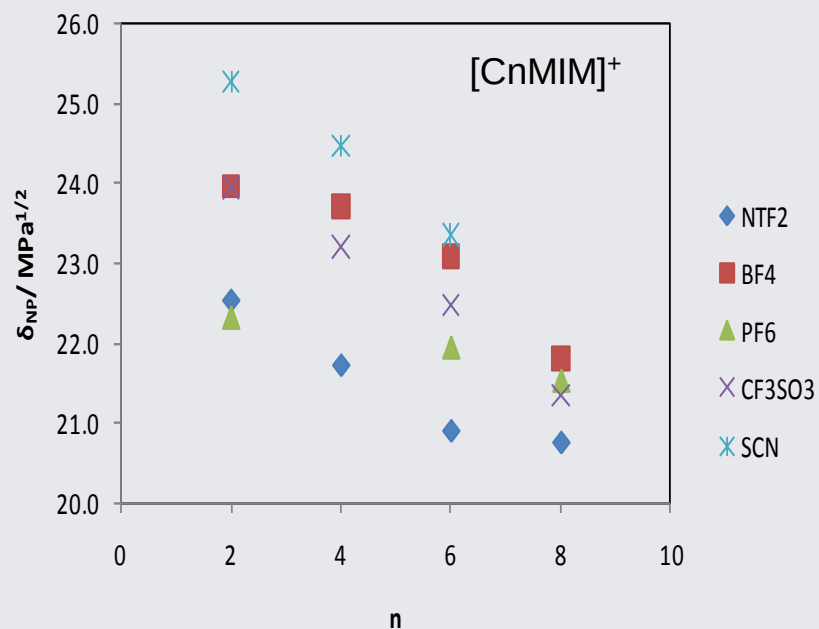
Data for δ_j and V_j were collected from literature at 298.15 K

Data for γ^∞ were collected from available data published at different temperatures

Estimation of Solubility Parameters

► Activity Coefficients at infinite dilution - Results & Discussion

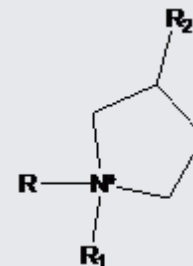
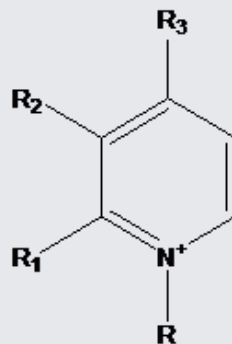
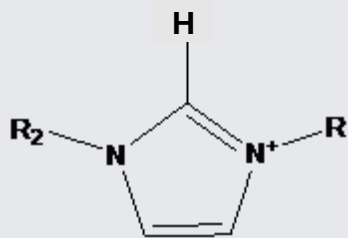
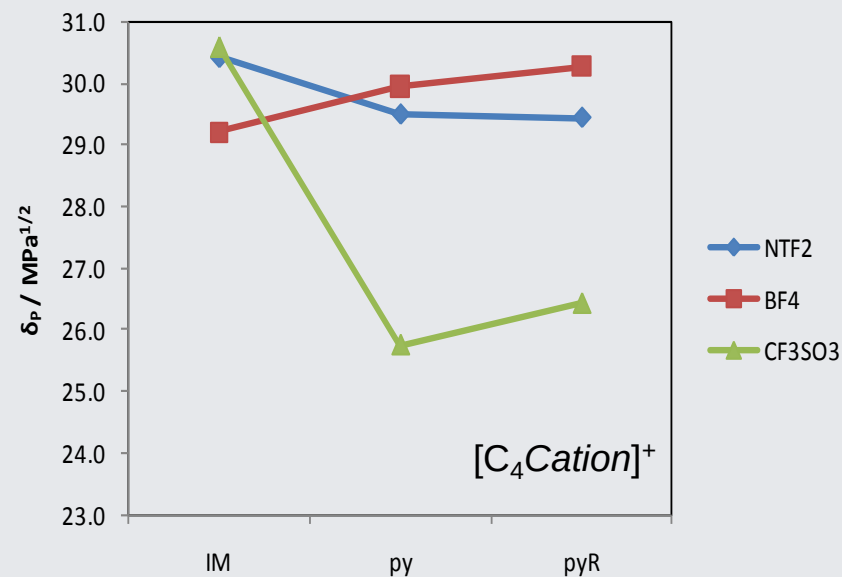
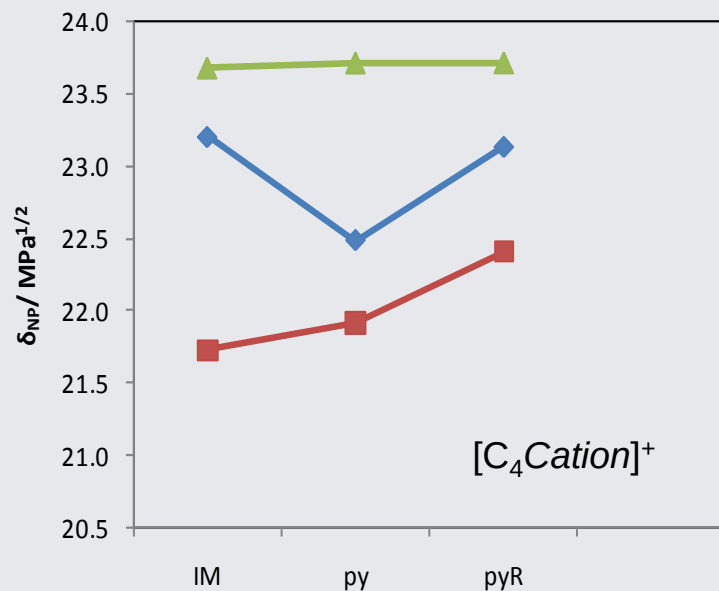
Alkyl chain length effect



Estimation of Solubility Parameters

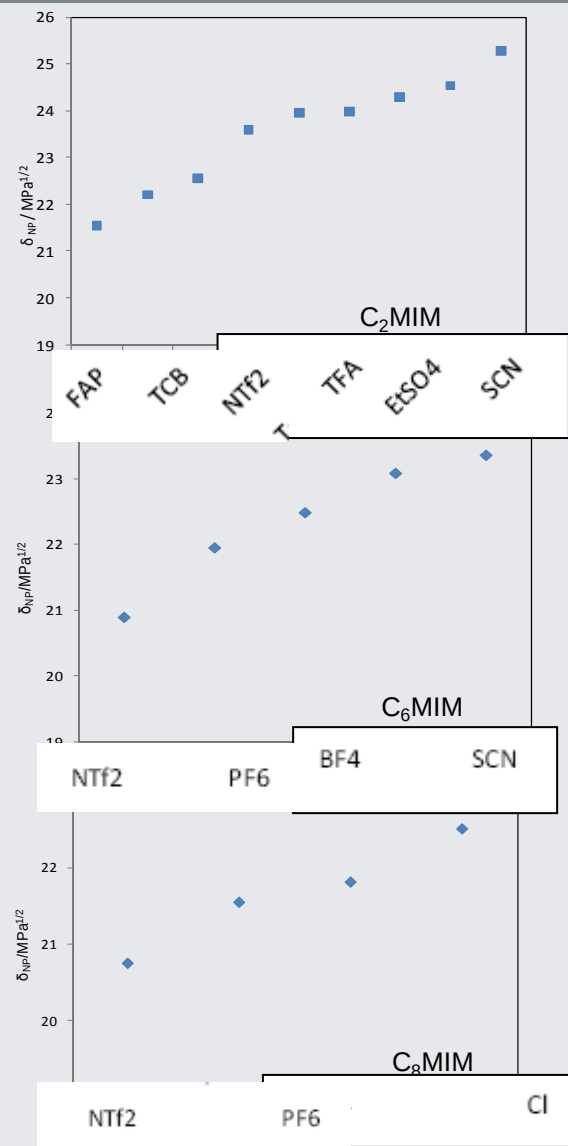
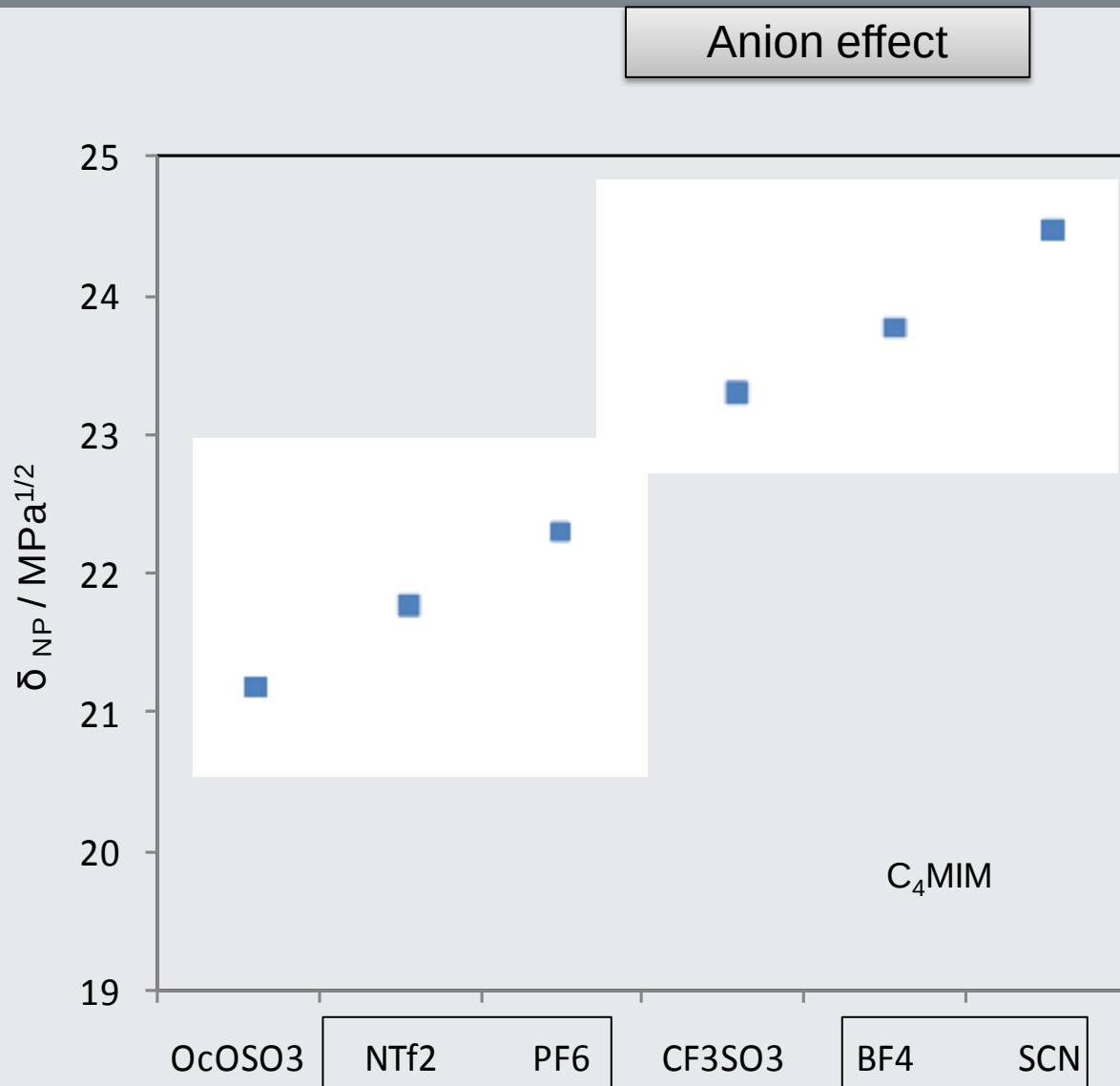
► Activity Coefficients at infinite dilution - Results & Discussion

Cation family effect



Estimation of Solubility Parameters

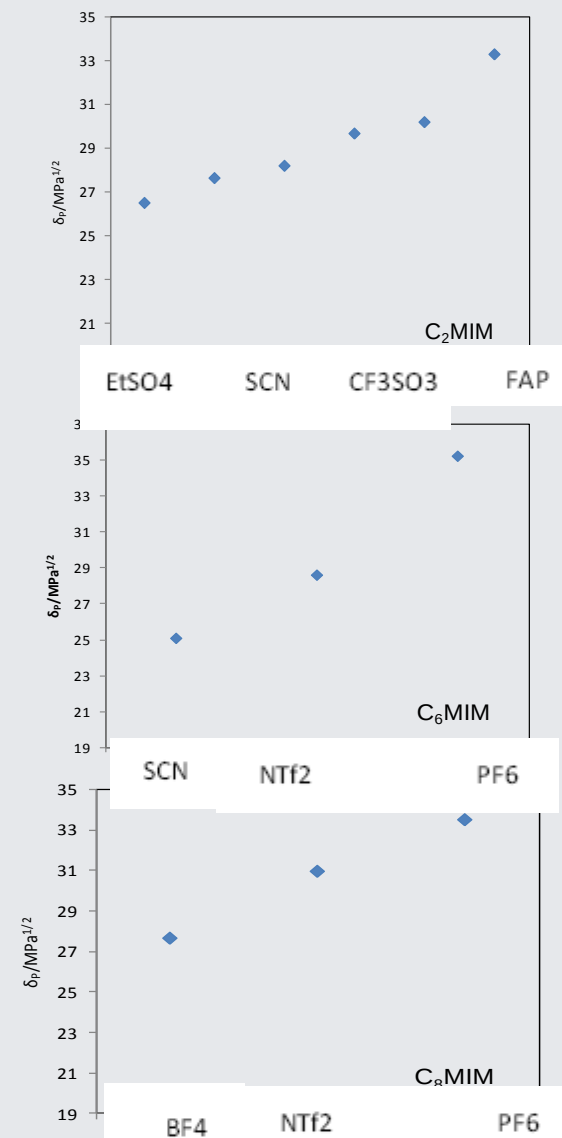
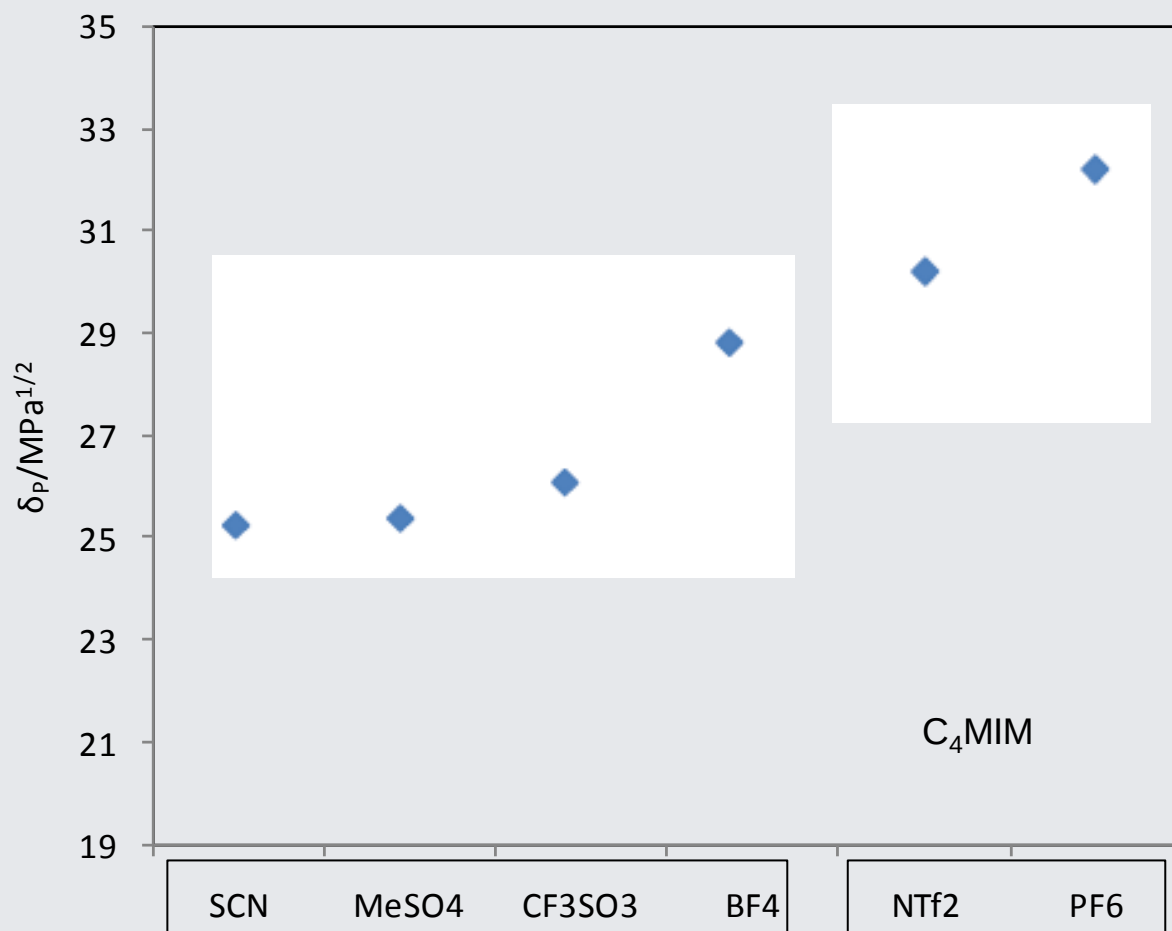
► Activity Coefficients at infinite dilution - Results & Discussion



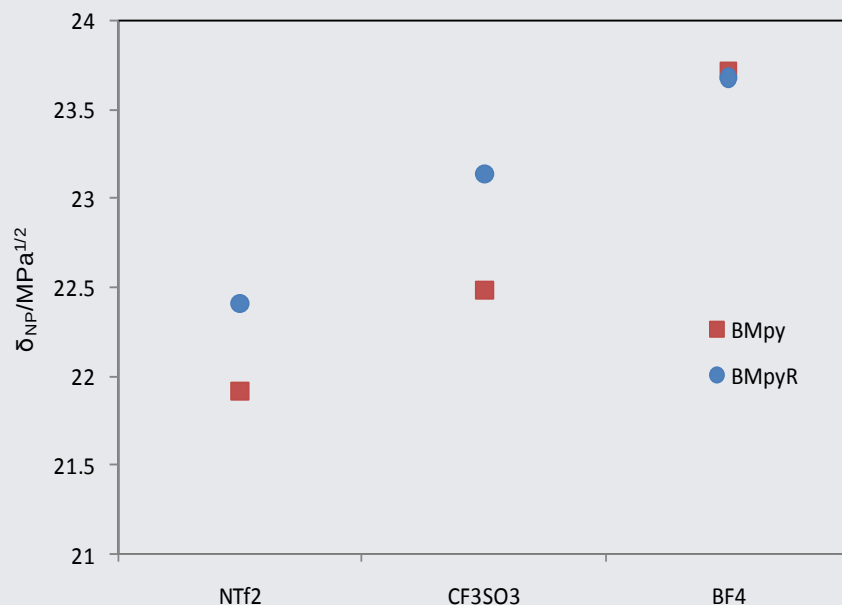
Estimation of Solubility Parameters

► Activity Coefficients at infinite dilution - Results & Discussion

Anion effect



Anion effect



► Viscosity

Kilaru, P.K. and P. Scovazzo, *Industrial & Engineering Chemistry Research*, 2008. **47**(3): p. 910-919.

$$\Delta G_{vis}^0 = RT \ln \left(\frac{\mu V_1}{h N_A} \right)$$

viscosity
with
molar energy of activation

$$E^{vap} = K_v \Delta G_{vis}^0$$

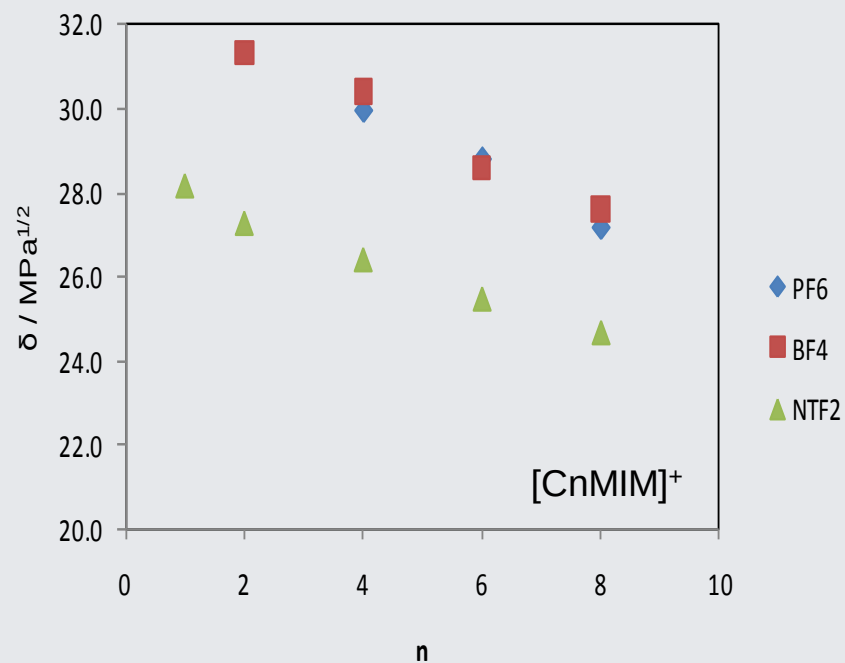
energy of vaporization
with
molar free energy of activation

$$\delta_1 = \left\{ \frac{K_v RT}{V_1} \ln \left[\frac{(1 \times 10^{-9}) \mu V_1}{h N_A} \right] \right\}^{1/2}$$

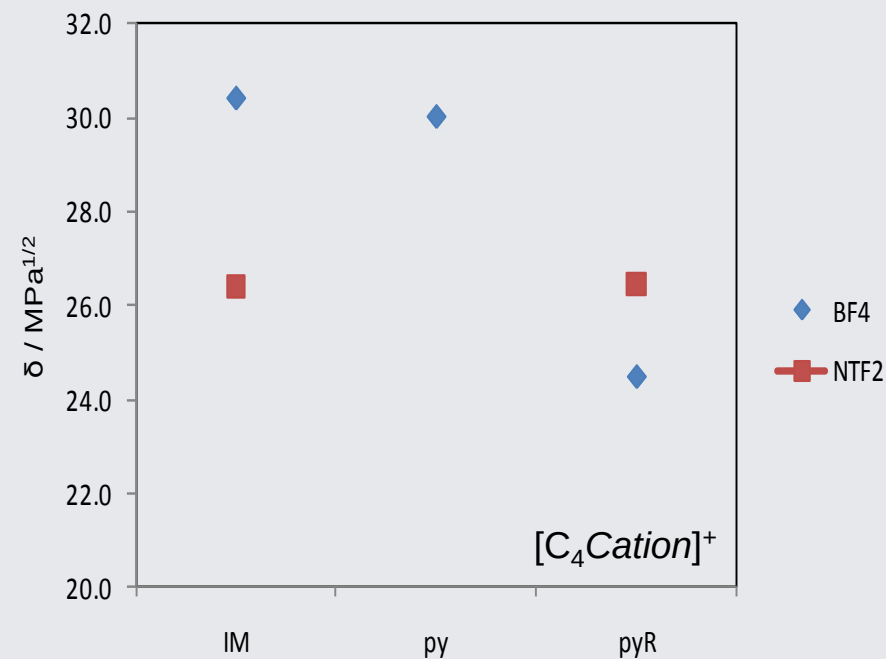
Solubility parameter for pure Ionic Liquid

► Viscosity - Results & Discussion

Alkyl chain length effect



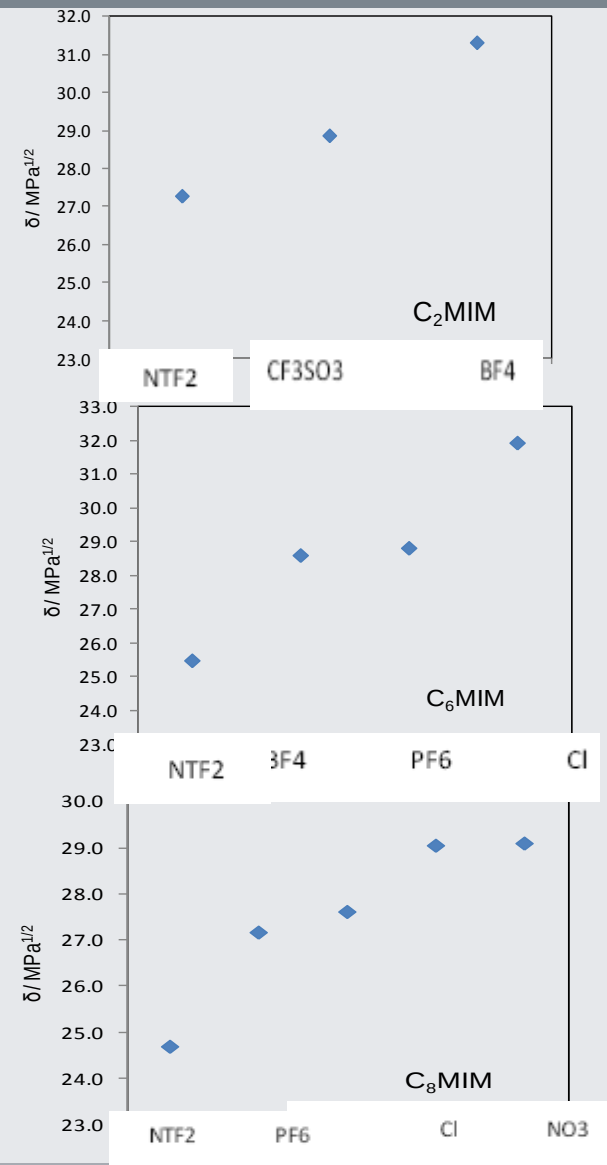
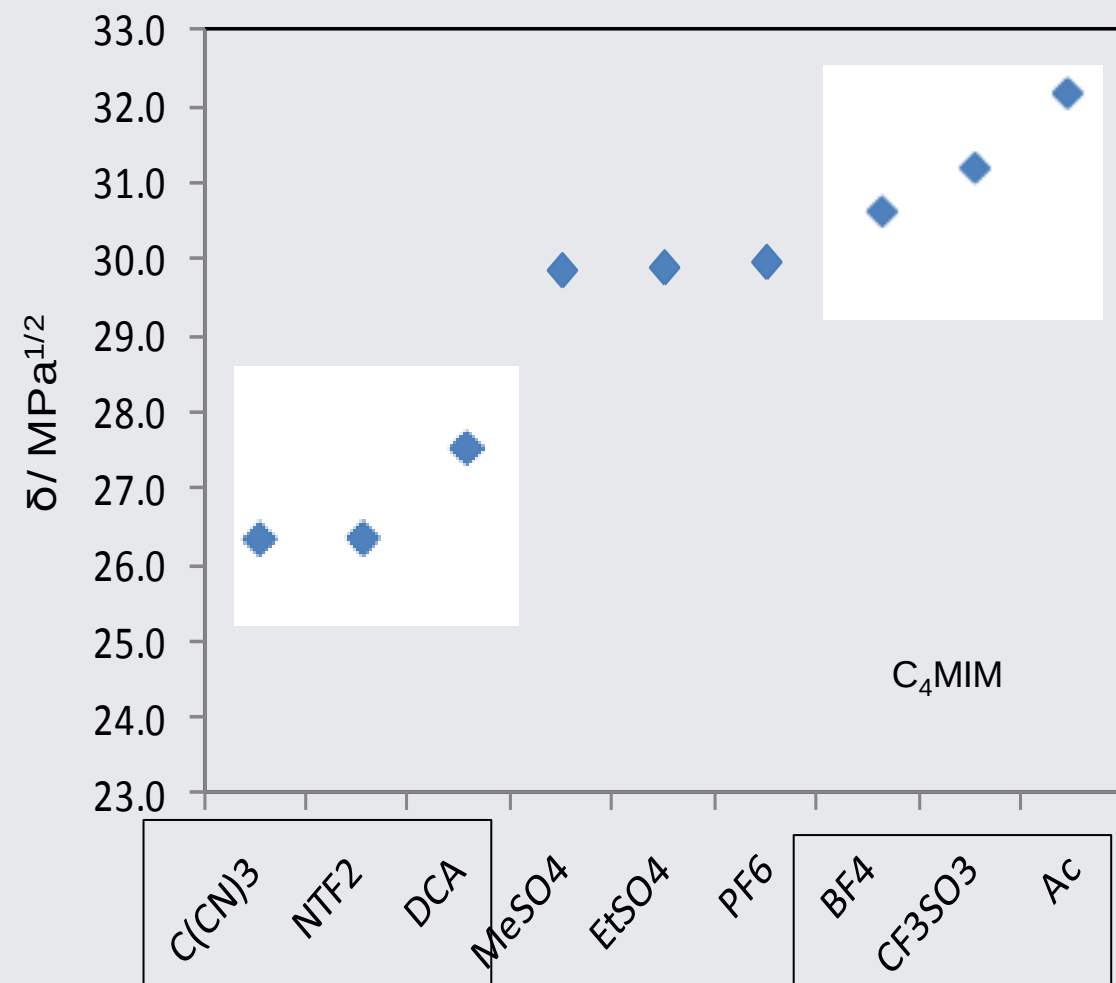
Cation family effect



Estimation of Solubility Parameters

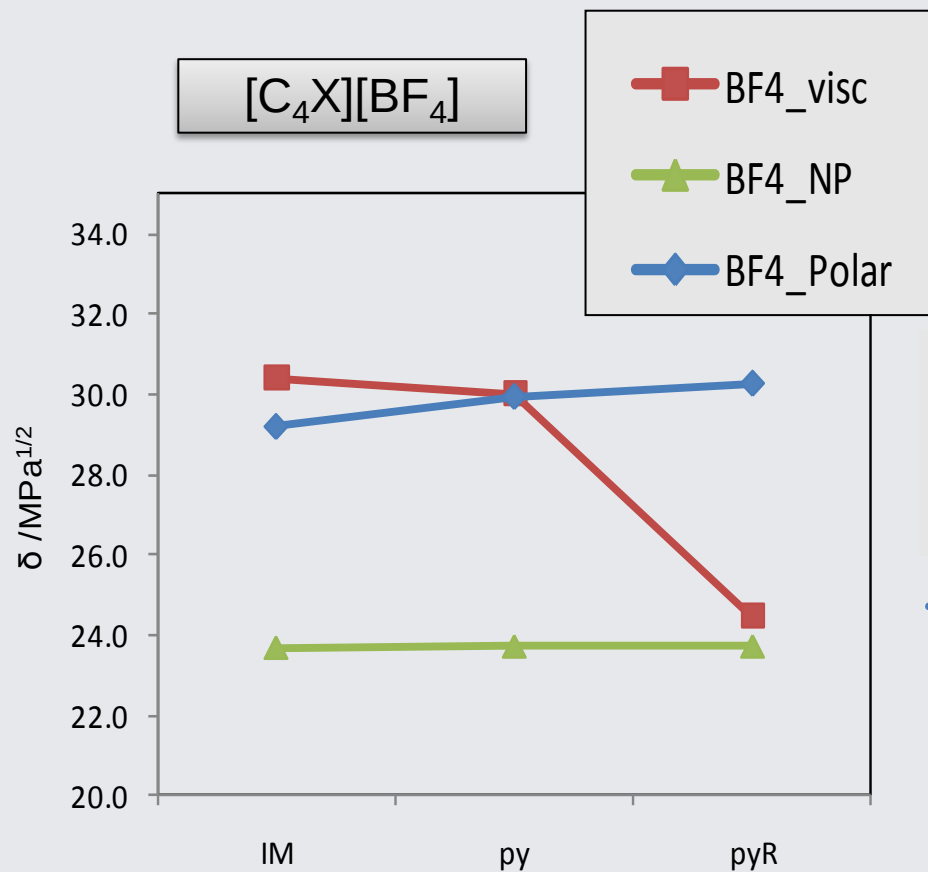
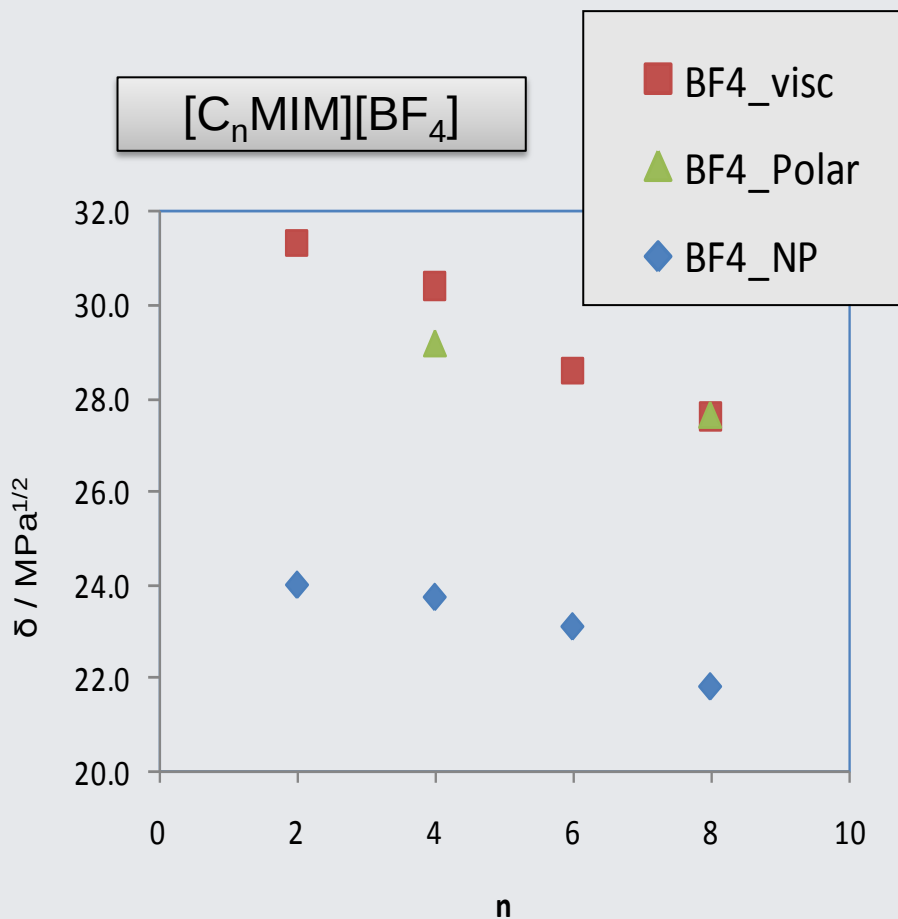
► Viscosity - Results & Discussion

Anion effect



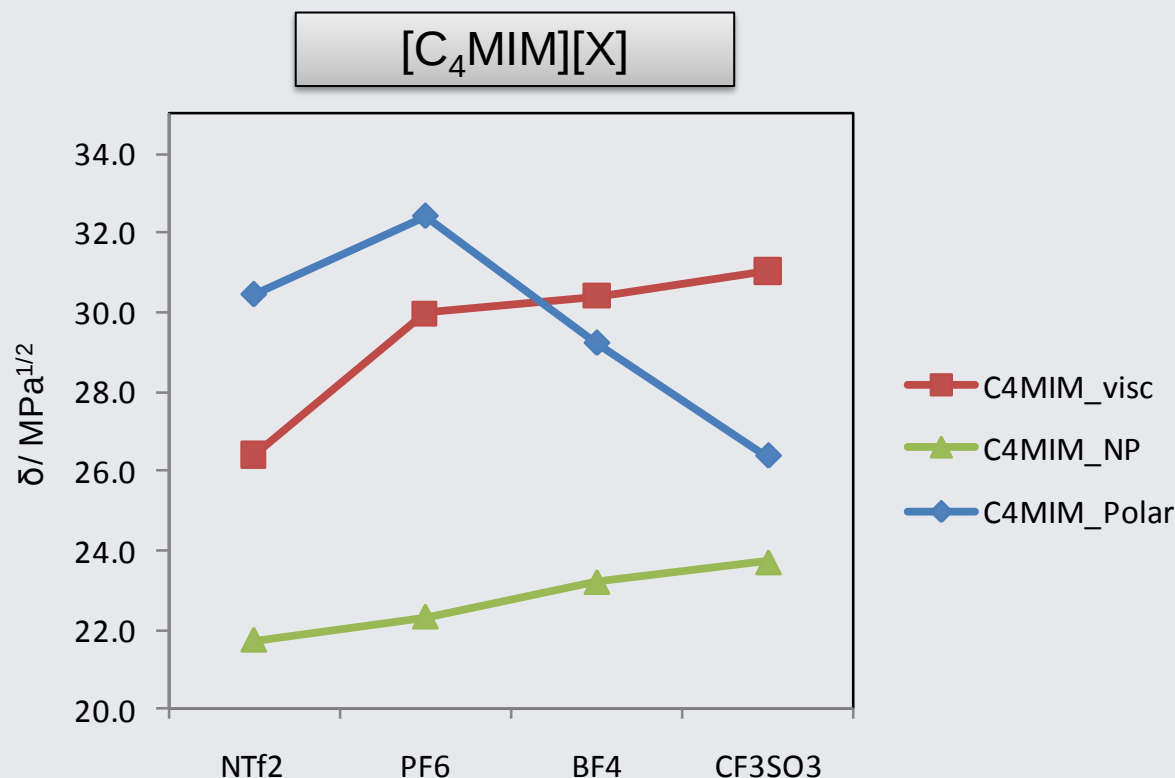
Estimation of Solubility Parameters

► Viscosity vs Activity coefficient at infinite dilution



2 Estimation of Solubility Parameters

► Viscosity vs Activity coefficient



- The values obtained for viscosity are closer to the solubility parameters for polar family
- The behavior is similar to solubility parameters for nonpolar family

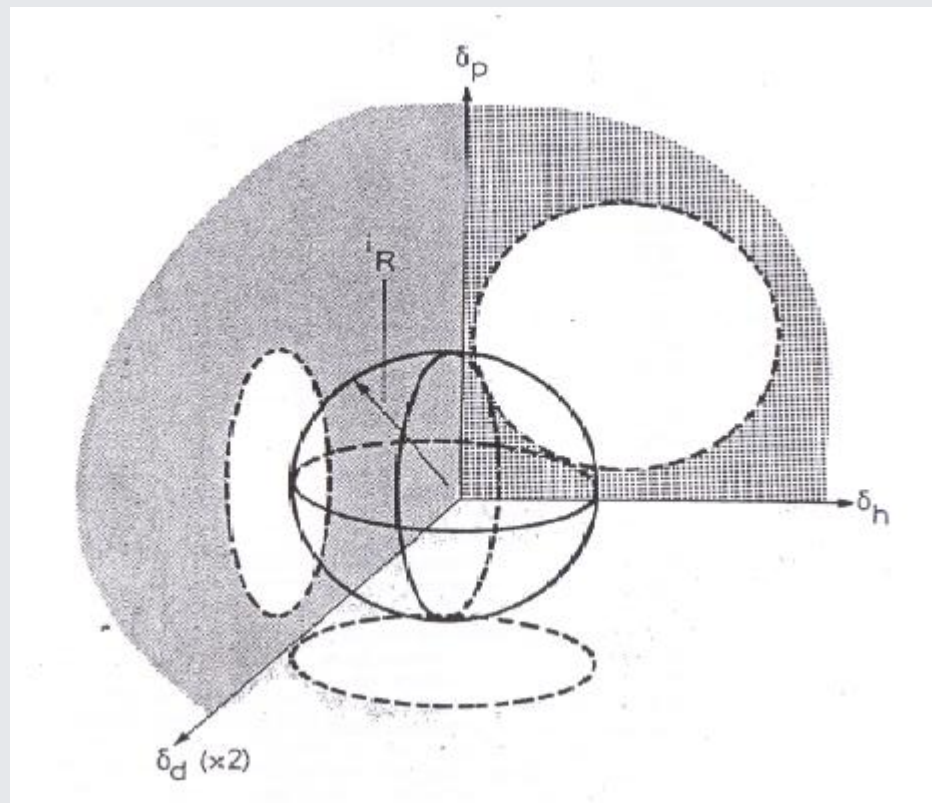
The regular solution theory, proposed by Hildebrand has proved to be useful to predict phase behaviour of solutions without detailing molecular polarity or specific interactions



Hansen

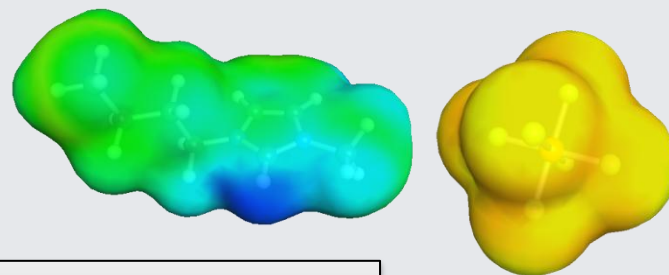
$$\delta_t^2 = \delta_d^2 + \delta_p^2 + \delta_h^2$$

Each interaction is accounted

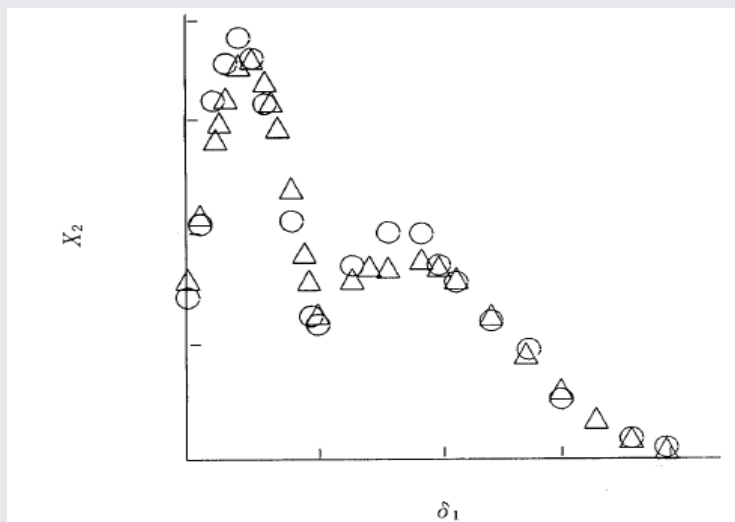


Experimental Section

Ionic Liquid in study:
 $[\text{C}_4\text{MIM}][\text{PF}_6]$



Determination of the solubility of this IL at mixtures with different compositions namely, 15, 30, 45, 60, 75 and 90% of 1-propanol and water, 1-propanol and toluene.



Experimental Section

IL in water and 1-propanol

UV



Experimental Section



IL in toluene and 1-propanol



Gravimetric Method

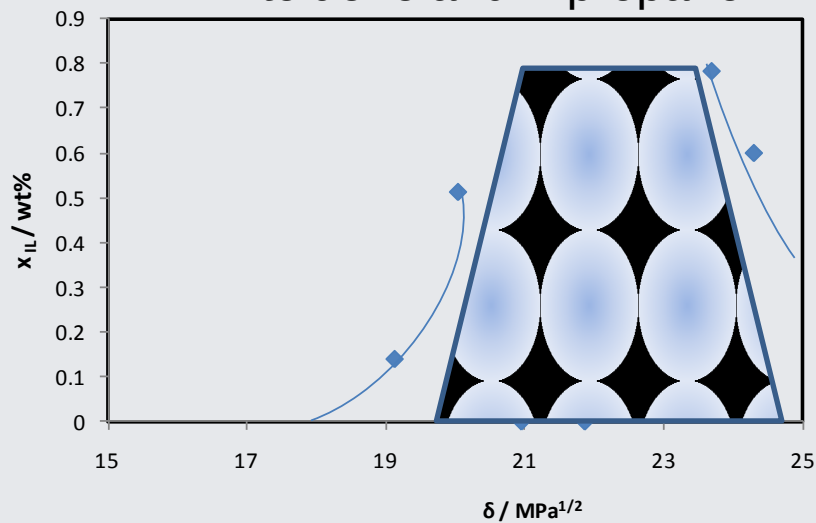


Experimental Section

Results and discussion

$$\delta = \sum f_i \delta_i$$

IL in toluene and 1-propanol



1-propanol / vv%	$\delta / \text{MPa}^{1/2}$	$x_{IL} / \text{wt\%}$
85	19.115	0.140
70	20.03	0.513
55	20.945	Miscible
40	21.86	Miscible
25	22.775	0.149
10	23.69	0.782
0	18.2	0.098

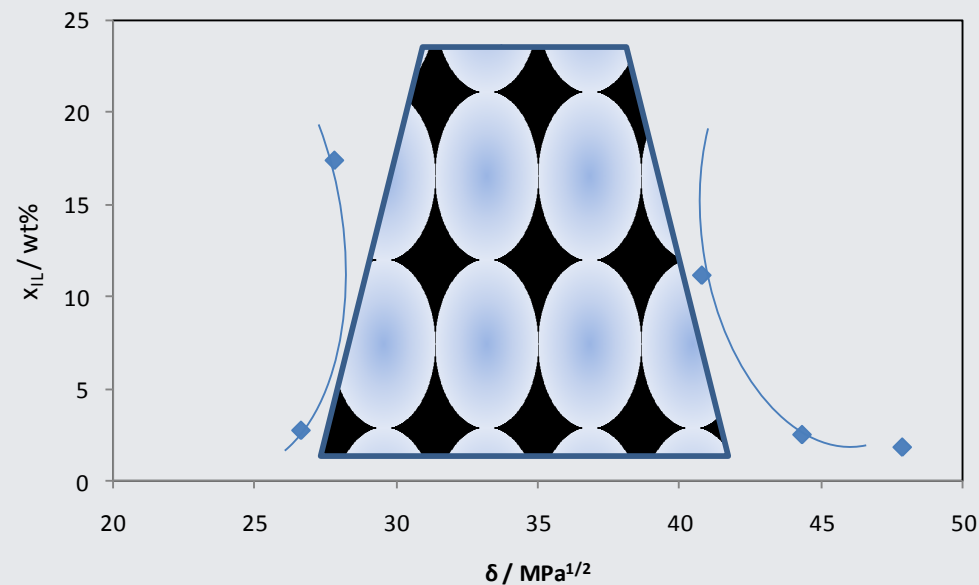
$\delta_{NP} = 22.34 \text{ MPa}^{1/2}$, $\delta = 29.98 \text{ MPa}^{1/2}$

Experimental Section

Results and discussion

$$\delta = \sum f_i \delta_i$$

IL in water and 1-propanol



1-propanol / vv%

$\delta / \text{MPa}^{1/2}$

$x_{IL} / \text{wt}\%$

0	47.9	1.875
15	44.36	2.556
30	40.82	11.202
45	37.28	12.030
60	33.74	23.204
85	27.84	17.435
90	26.66	2.787
100	24.3	0.600

$\delta_P = 32.4 \text{ MPa}^{1/2}$, $\delta = 29.98 \text{ MPa}^{1/2}$

- ❖ An **amphiphilic (Chamaleonic) behavior** of the ILs is observed when solubility parameters are estimated from activity coefficients at infinite dilution;
- ❖ The use of viscosity to estimate the solubility parameter shows that pure ILs **act predominantly as a polar molecules**. Values for solubility parameters equivalent to those obtained in presence of polar solvents are obtained;
- ❖ Solubility measurements **confirm the behavior** observed with infinite dilution activity coefficients;
- ❖ It is shown that the Hildebrand solubility parameters (unidimensional) cannot adequately describe the ILs behavior; The use of the Hansen's approach is suggested.

Given the complexity of interactions, for future work it would be interesting to work in the solubility parameters through Hansen's theory which takes accounts three different contributions,

$$\delta_t^2 = \delta_d^2 + \delta_p^2 + \delta_h^2$$

Acknowledgements

❖ Professor João A.P Coutinho

❖ Path group